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Author post-print (accepted) deposited by Coventry University's Repository

## Original citation & hyperlink:

Badawy, T, Hamza, M, Mansour, MS, Abdel-Hafez, AHH, Imam, H, Abdel-Raheem, MA, Wang, C & Lattimore, T 2019, 'Lean partially premixed turbulent flame equivalence ratio measurements using laser-induced breakdown spectroscopy' *Fuel*, vol. 237, pp. 320-334.

<https://dx.doi.org/10.1016/j.fuel.2018.10.015>

DOI 10.1016/j.fuel.2018.10.015

ISSN 0016-2361

Publisher: Elsevier

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# Lean partially premixed turbulent flame equivalence ratio measurements using Laser-induced breakdown spectroscopy

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## Abstract

The creation of a more stable flame along with the extension of flammability limits under lean mixture combustion was the main motivation to develop a new burner design, which has been investigated in this research. The current burner configuration was utilized to create a wide range of higher turbulent intensities and to produce different degrees of mixture inhomogeneity, which acted to promote minimum pollution, highest performance and higher flame stability. The burner stability assessment was investigated using two types of fuel: natural gas (NG) and liquefied petroleum gas (LPG). They were tested under different degrees of partial premixing, and two turbulence generator disks for lean mixture at an equivalence ratio of  $\varphi = 0.8$  were used. Following this, the Laser Induced Breakdown Spectroscopy (LIBS) technique was utilized to characterize and quantify the impact of changing the disk slit diameter on the distributions profiles of equivalence ratio or mixture fraction for a NG/air partially premixed flame. A series of homogeneous NG/air mixtures with different equivalence ratios were used to obtain the correlations between the measured emission lines of LIBS spectra and the global flame equivalence ratio. Consequently, the emission spectral lines ratios of H/N, H/O and C/N+O were utilized to predict the equivalence ratio distributions. The results demonstrated that for all of the mixing lengths, NG/air mixture with larger disk generator diameter yielded the maximum burner stability, whilst the LPG/air mixture with a larger disk generator diameter resulted in the minimum burner stability. Furthermore, the flame associated with the larger disk slit diameter had a uniform local equivalence ratio distribution and lower RMS fluctuation profiles of equivalence ratio in comparison to the lower disk slit diameter.

**Keywords:** Stability; laser breakdown; partially premixed; Turbulence; LIBS; Mixture fraction

## Highlights:

- Fuel type and partially premixed level effects on burner stability
- Flame stability behaviour of different turbulence generator disks were investigated
- Impact of changing the disk slit diameter on equivalence ratio distributions was examined

## Nomenclature

LIBS	laser induced breakdown spectroscopy	$Y_{fi}$	Mass fractions of the fuel elements
$d_s$	Turbulence generator diameter	$L_k$	Kolmogorov scale
$\xi$	Mixture fraction	HI	Hydrogen intensity
NG	Natural gas	$\lambda$	Laser wavelength
PPFs	Partially Premixed Flames	$V_j$	Jet velocity
ICCD	Intensified Charge-coupled device	$\tau_{mix}$	Mixing time
L	Mixing length, mm	$\varphi$	Equivalence ratio
b	Slit thickness	$d_c$	Cone diameter
LTE	Local Thermal Equilibrium	X	Axial distance above the burner tip
$C_3H_8$	Propane	$C_4H_{10}$	Butane
Rms	Root mean square	$\delta$	Convection-diffusion laminar flame thickness
PI	Princeton Instruments	OI	Oxygen intensity
NI	Nitrogen intensity	$\theta$	Cone half angle
CI	Carbon intensity	d	Inner diameter of the inner tube, mm
D	Inner diameter of the outer tube, mm	do	Outer diameter of the inner tube, mm
Do	Outer diameter of the outer tube, mm	X	Axial distance, mm
r	Radial distance, mm		
R	Inner radius of the outer tube, mm		

## Introduction

The mixture stratification process and the generation of higher turbulence levels are the two main established techniques to extend the lean combustion limit [1]. Therefore, the new combustion system design, directed towards partially premixing combustion, is a promising technology, which offers the potential to meet ever stringent emission regulations, as well as improving the system efficiency [2]. The performance of the combustion processes is mainly linked to the local equivalence ratio distributions near the ignition event, and based on these distributions, the combustion characteristics and the level of emissions such as CO, NO<sub>x</sub>, etc. will be strongly affected [3, 4]. This influence is mainly linked to the change of both the local properties of the reaction zone and the global behaviour of the combustion system associated with the flame propagation within spatial variations of the equivalence ratio [5]. Therefore, quantifications of this ratio are essential to sustain the higher stability of the combustion process and to minimize the soot emissions [6].

Richardson et al. [7] demonstrated that the laminar flame propagation speed was affected by the equivalence ratio gradients, due to the gradients effects on the molecular transport of hot products and radical species into the reaction zone. Furthermore, Dold [8] concluded that as the mixture fraction or equivalence ratio gradient increased, the flame propagation speed was reduced. This was attributed to the lower conduction heat transfer associated with the increased flame front curvature, which consequently reduced the preheating process of the unburned mixture. Likewise, Richardson and Chen [4] investigated turbulent flame propagation under the impacts of equivalence ratio-stratification for methane air flame using DNS analysis. They concluded that the stratification process influences significantly on the flame surface area due to the variation caused by equivalence ratio gradient orientation on the flame surface averaged consumption speed with surface averaged equivalence ratio.

In order to measure and obtain comprehensive information regarding global and local equivalence ratios distributions in turbulent flames, laser induced break down spectroscopy (LIBS) was used in this research. The principle of laser induced breakdown spectroscopy depends mainly on the interaction of a very short-duration focused pulsed laser beam onto the surface of the substance to be analysed, causing the breakdown of the sample's chemical bonds, followed by the formation of plasma, which is composed of ionized matter [9, 10]. During the subsequent relaxation of the constituent excited species, the spectral emission occurred, and it was collected and spectrographically analysed using an Intensified CCD (ICCD) detector attached to a spectrograph detector [11]. The elemental composition of any material can be identified based on their fingerprint spectral lines, and consequently, the concentration of such elements will be quantified from the spectral line intensities. The main advantages of the LIBS technique lies in its ability to rapidly analyse samples remotely and in situ, with minimal sample preparation [12, 13]. Furthermore, LIBS has the potential of simultaneous multi-elemental analysis with minimum equipment [14]. The aforementioned advantages make the LIBS technique to an attractive tool for the majority of applications including liquids [15, 16], solids [17, 18] and quantitative analysis of gases and gas mixtures, which are all essential tasks in the field of security, environmental and chemical analysis [19, 20].

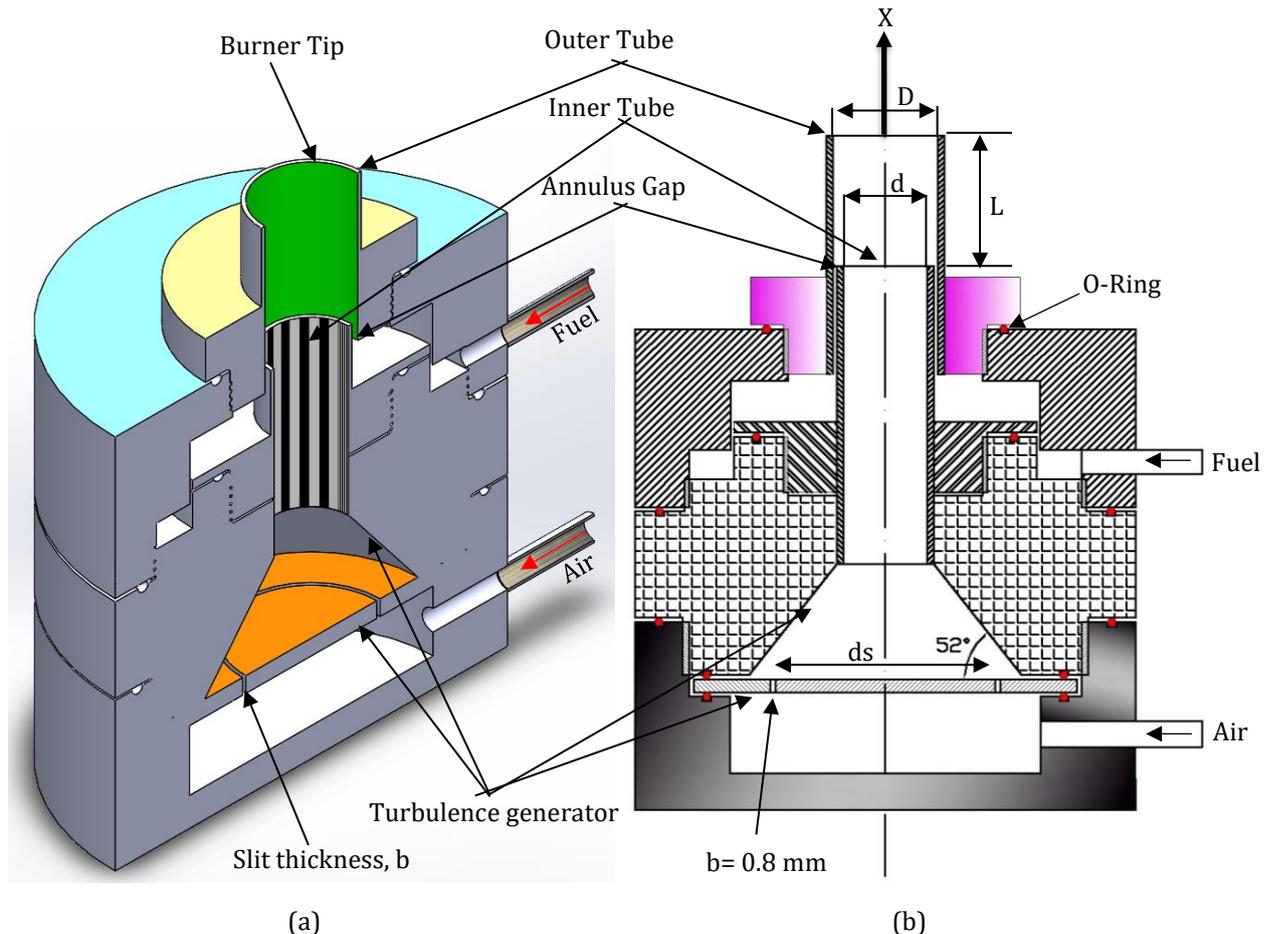
Over the past few years, the LIBS technique has been applied extensively to the field of combustion diagnostics [21, 22] for equivalence ratio measurements which can be obtained based on the atomic species concentrations in flames. Kotzagianni et al. [23] established a new calibration scheme for equivalence ratio measurements of non-premixed and premixed methane turbulent flames using the LIBS technique. They concluded that for a lower mole fraction of methane in the range 0-0.3, the ratio of H $\alpha$  (656.3 nm) over O (777.3 nm), (H $\alpha$ /O), should be utilized for equivalence ratio calculations. Additionally, they found that, for a higher mole fraction of methane in the range 0.3-1, the ratio of C<sub>2</sub> over CN, (C<sub>2</sub>/CN), should be used to identify the equivalence ratio. The majority of past LIBS studies were mainly focused on using the ratios of some spectral lines of the atomic origin, such as the carbon line to nitrogen [C (833 nm)/N (744 nm)], the carbon line to oxygen [C (833 nm)/O (777 nm)] [24], or the ratio of the intensity of a carbon line to the sum of the intensities of a nitrogen and an oxygen line, [C (711 nm)]/[N (744 nm) + O (777nm)] [25]. These ratios have been successfully utilized to delineate the relationship between the spectral intensity and the mixture equivalence ratio. The most commonly used ratios were between the hydrogen line to an atomic emission of oxygen line [H $\alpha$  (656.3 nm)/O (777nm)] or hydrogen line to an atomic emission of nitrogen [H $\alpha$  (656.3 nm)/N (746.8nm)] [26-28]. Alongside the equivalence ratio measurements, LIBS has been utilized for further analysis of the turbulent flame characteristics, including the measurements of temperature [28], gas density and concentration [29].

The present work discusses the development of a new burner design, which has the ability to operate over lean combustion conditions with higher flame stability, and consequently, it provides lower levels of

106 exhaust emissions. This burner generates different stratification degrees of the mixture by changing the  
 107 degree of the partially premixed level or by using different turbulent generator disks. Considerable  
 108 attention has been paid to obtain comprehensive information regarding the impact of changing the disk slit  
 109 diameter, fuel type and the level of partially premixed on the flame stability maps. The stability map results  
 110 were examined and utilized to identify the suitable mixture conditions for equivalence ratios distributions  
 111 using the LIBS technique. Likewise, the ability to conduct quantitative equivalence ratio measurements of  
 112 partially premixed NG/air mixtures using the LIBS technique was examined. Furthermore, the correlation  
 113 of values of emission intensity ratio  $[C/(N+O), H/O \text{ and } H/N]$  using LIBS against NG/air mixtures  
 114 equivalence ratios was established.  
 115

## 116 2.1. Burner setup details

117  
 118 The new design of the current burner configuration was comprised of a pair of fixed concentric stainless-  
 119 steel tubes; the inner tube carried the air whilst the outer tube carried the fuel, as shown in Figure 1.



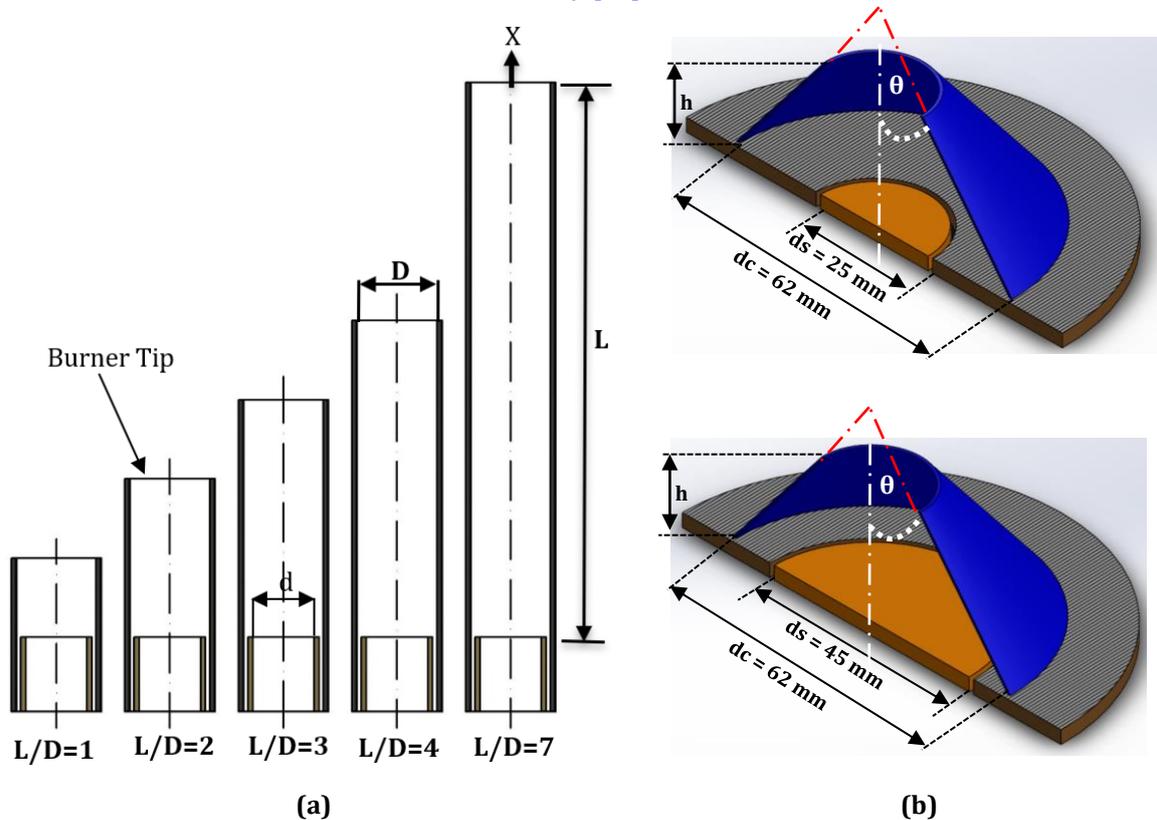
120 Figure.1. Burner schematic diagram (a) half section 3D sketch, (b) half section 2D sketch  
 121

122 This new burner has the strength to generate higher levels of turbulence intensities as well as the ability to  
 123 provide different degrees of partial premixing. The inner tube has a wall thickness of 1.5 mm and an inner  
 124 diameter of  $d = 19$  mm, whilst the outer tube has a wall thickness of 1.5 mm and an inner diameter of  $D =$   
 125  $24$  mm. The outlet of the inner tube was located at a distance  $L$  below the tip of the outer tube. The mixing  
 126 process between air and fuel occurred within this distance  $L$ , and consequently, by changing this distance,  
 127 the degree of inhomogeneity was varied. The degree of partial premixing was defined by the ratio  $L/D$  and  
 128 five sets of  $L/D = 1, 2, 3, 4$  and  $7$  were selected to investigate the burner stability as shown in Figure 2 (a).  
 129 Both the air and fuel streams were fed into the burner tangentially and directed towards the inner and  
 130 outer tubes, respectively. The fuel stream passed through the annulus gap between the vertical concentric  
 131 tubes and then it mixed with the air through the mixing distance,  $L$ , as shown in Figure 1. The LPG used  
 132 during the present study was formed of 50% butane and 50% propane (molar basis). While the NG was  
 133 formed from of 95% methane (molar basis). The flow rates of both air and fuel streams were controlled  
 134 precisely using an Alicat MCS-series meter which was calibrated to a certain range of 150 l/min with a high  
 135 accuracy of  $\pm (0.4\% \text{ of Reading and } + 0.2\% \text{ of Full Scale})$ . Additionally, it had a 10-millisecond response

136 time. Both the fuel and air streams were introduced to the burner at ambient conditions. The overall mean  
 137 equivalence ratio was determined based on the fuel and air stream mass flow rates.  
 138

## 139 2.2. Turbulence generator disks

140  
 141 The turbulence generator used for the current study consisted of a thin disk turbulence generator with a  
 142 circular slot, in order to boost the turbulence intensity levels, similar to the disk developed by Videto and  
 143 Santavicca [30]. Beyond this disk, a contracting nozzle was utilized to assist the collapse of the air stream,  
 144 which passed through the circular slot, into a wide range of turbulent fluctuations and integral length scales,  
 145 and consequently, this promoted higher levels of turbulence intensities [31]. Recently, several studies have  
 146 been conducted to develop new turbulence generator designs in order to increase the turbulent flame  
 147 speed and to achieve improved flame stability [32]. In this paper, two disks with a circular slit diameter of  
 148  $d_s = 25$  and  $45$  mm have been selected, as shown in Figure 2 (b). Both the disks were designed with a  
 149 constant slit thickness ( $b$ ) of  $0.8$  mm, whilst the following converging nozzle consisted of a cone angle ( $2\theta$ )  
 150 of  $76^\circ$ ,  $26$  mm height ( $h$ ) and  $62$  mm base cone diameter ( $d_c$ ). At a partial premixing level of ( $L/D = 2$ ), a  
 151 particle image velocimetry (PIV) system was utilized to study the velocity profiles of the developed burner.  
 152 Accordingly, the flow turbulent intensities were calculated as a ratio between the fluctuation of the jet  
 153 velocity to the mean jet velocity ( $V_{rms}/V_j$ ) [33]. They demonstrated that the current burner turbulent  
 154 intensity could reach up to  $36\%$ , depending on the jet velocity, and any increase in the jet velocity or the  
 155 disk slit diameter will increase the turbulent intensity [33].

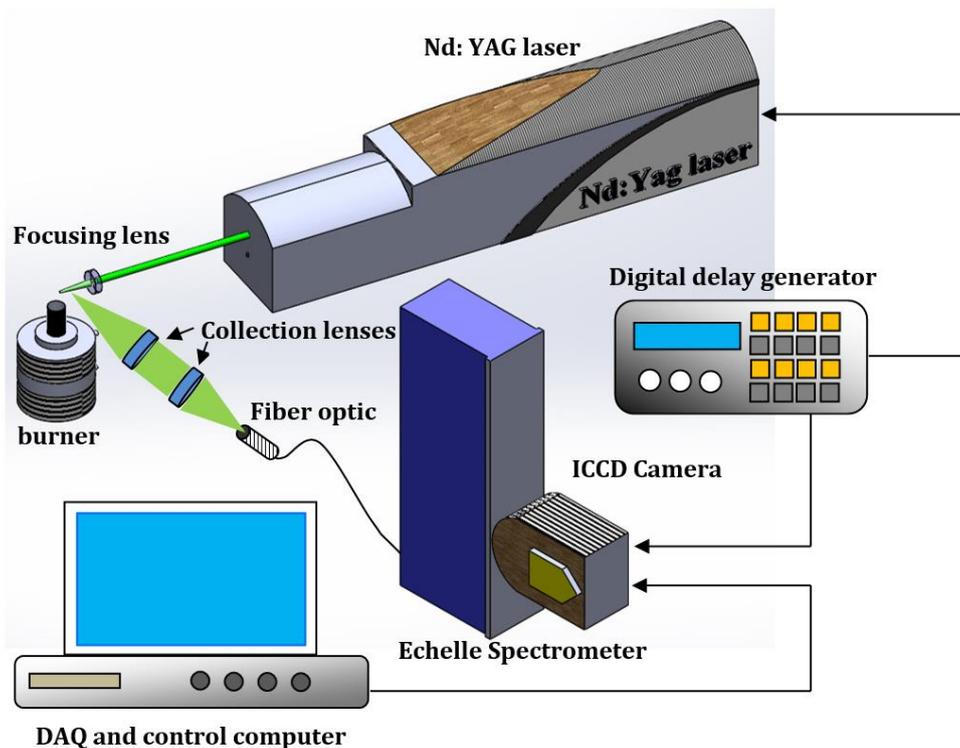


156  
 157 **Figure.2.** (a) Sets of 5 different levels of partial premixing ( $L/D$ ), and (b) Different slit diameters ( $d_s = 25$   
 158 mm and  $45$  mm) used for the turbulence generator disks

## 159 2.3. LIBS set-up

160 The schematic diagram of the experimental apparatus used for the LIBS-technique is presented in Figure  
 161 3. The plasma was generated by using a pulsed Nd: YAG laser with a frequency of  $10$  Hz. This laser beam  
 162 was characterised as the first harmonic wavelength of  $1064$  nm, pulse width of  $6$  ns and a beam diameter  
 163 of  $10$  mm. Single shot operations of the laser were used for the current investigation, with a constant laser  
 164 energy of  $100$  mJ, whilst the focusing process of the laser beam was carried out using a  $50$  mm focal length  
 165 plano-convex lens to create the plasma. This plasma constitutes of excited atoms in the ionized gas, and  
 166 during the subsequent decay of the excited electrons, a rainbow of light of different wavelengths is released,  
 167 resulting in characteristic spectral emissions. In order to optimize the spectral emission data collections, a  
 pair of  $100$  mm focal-length plano-convex lenses were placed at an angle of  $26^\circ$  to the laser beam [9], and

168 then the spectral emissions were directed towards a fused-silica optical fiber with an aperture of 200  $\mu\text{m}$ .  
 169 Consequently, the spatial resolution of the system based on this aperture diameter was small enough for  
 170 turbulent flame measurements and it was approximately 1 mm, estimated from the size of the plasma.  
 171 Consequently, the optical fiber captured the emitted light and it carried it to an Echelle spectrometer (PI-  
 172 Echelle, Princeton Instruments: IMAX-512, USA) attached to a gated Intensified Charge-Coupled Device  
 173 (ICCD) covering a wavelength range of 190–1100 nm, to resolve and image the signal spectrally. The data  
 174 acquisition system was utilized to precisely control both the gate delay time and the gate width of the  
 175 spectroscopic data acquisition system. In order to achieve high measurement accuracy, the laser induced  
 176 plasma generated should reach the Local Thermodynamic Equilibrium (LTE) state, and for the current  
 177 investigation, the LTE was established at roughly 1  $\mu\text{s}$  following the plasma initiation.



178 **Figure.3.** Schematic diagram of the LIBS setup

179  
 180 A Stanford research model DG535 4-channel delay pulse generator was employed to precisely control the  
 181 Shutter timing of the ICCD camera and the laser-trigger signals. A precise control of the timing parameter  
 182 and delay time was carried out by combining the fast oscilloscope (500MHz) with the fast photodiode (rise  
 183 time = 1 ns). The spectral emission lines were analysed and identified using commercial software  
 184 (GRAMS/Alv.8.0, Thermo-electron. Co.). The raw emission signals collected by the LIBS system were  
 185 corrected by subtracting them from the emission background by using the LIBS software (Winspexs 21).  
 186 This correction was applied to eliminate the inherently dark signal associated with the spectrometer  
 187 detector, which itself is associated with the output LIBS signal. Both the delay time and the gate width were  
 188 varied until the optimized intensity of the spectral emission line was obtained. In order to achieve that  
 189 optimized signal, the ICCD gate width was set at 10,000 ns, whilst the spectral emission line intensities  
 190 were collected at a delay time of 600 ns after the laser irradiation. For the present work, one case was  
 191 selected for equivalence ratio measurements using the LIBS technique. The NG/air mixture employed for  
 192 this case study was characterized by an equivalence ratio of  $\phi = 0.8$ , mass flow rate of 2.91 kg/h and jet  
 193 velocity of  $V_j = 1.6$  m/s. A long distance pipe, with an approximate length of 200 times the pipe diameter  
 194 was selected for the fuel-air mixing process, to create a perfectly homogeneous mixture valid for precise  
 195 calibration with the LIBS technique. Consequently, the equivalence ratio measurements were carried out  
 196 using the LIBS technique after the calibration process was completed.

198 **3. Results and discussion**

199 **3.1. Stability limit characteristics**

200 **3.1.1 Stability limit characteristics for each fuel and each disk**

201 The degree of mixture stratification at the exit of the outer tube of the current burner is affected by changing  
202 the mixing length to diameter ratio ( $L/D$ ) and by varying the turbulence generator disk slit diameter.  
203 Consequently, these equivalence ratio fluctuations will influence the stability, dynamics and the structure  
204 of the flame [34]. Therefore, the flame stability behaviour can be characterized, with particular respect to  
205 the blowout characteristics to delineate the extinction regions between different Reynolds numbers and  
206 either the degree of partial premixing ( $L/D$ ) or the equivalence ratio,  $\phi$ . The blowout limit is identified by  
207 the bulk jet velocity,  $V_j$  at which a complete flame extinction is occurs. This extinction is carried out by  
208 increasing the air flow rate while keeping the fuel flow rate fixed, whereas, the blowout limits are obtained  
209 only from visual inspection of the flames [35].  
210

211 In the present work, the assessment of the burner stability was implemented at lean conditions of  $\phi = 0.8$   
212 for five sets of partial premixing ratios ( $L/D = 1, 2, 3, 4$  and  $7$ ) as shown in Figure 4 (a). The investigation of  
213 the stability map was accomplished for two types of fuels, NG and LPG, using two turbulence generator  
214 disks with slit diameters of  $d_s = 25$  and  $45$  mm. At  $L/D = 1$ , the flame was considered nearly non-premixed,  
215 while at  $L/D = 7$ , the flame was considered almost fully premixed. Furthermore, qualitative measurements  
216 of flame characteristics such as flame shape, height and colour associated with each case have been  
217 observed as shown in Figure 4 (b). Five rows of images, which represent a comparison between LPG, and  
218 NG, for each disk slit diameter, at different degrees of partial premixing, are presented. It was noticed from  
219 Figure 4 (a), that changing the degree of partial premixing or changing the turbulent generator disk slit  
220 diameter has a significant effect on the flame stability for both fuels. At  $L/D = 1$ , the NG/air mixture for both  
221 the disk slit diameters exhibited the maximum flame stability, whilst the LPG/air mixture with  $d_s = 45$  mm  
222 demonstrated the minimum flame stability. These results are further explained with the flame images,  
223 where NG demonstrated a stable flame with a blue colour, whilst LPG showed a significant small blue region  
224 near the flame base followed by a bright yellow flame with high luminosity. The LPG flames look more like  
225 diffusion flames, and consequently, the longer flame height associated with LPG flames can be linked to the  
226 flame elongating, to obtain the oxygen available in the ambient air. The blue flame near the base is due to  
227 the enhanced local partial premixing. The lower stability of LPG/air mixture in comparison to the NG/air  
228 mixture could be attributed to the different properties of the fuels, in particular the Lewis number. As it is  
229 well known, both the local stretch rate and the physicochemical parameters including the Lewis number  
230 and the laminar burning speed have a significant influence on the turbulent burning speed [36]. Clarke [37]  
231 calculated the Lewis number against the equivalence ratio for a range of different fuel-air mixtures that are  
232 in common use. For lean mixture conditions, the Lewis number for NG ( $Le = 0.94 @ \phi = 0.8$ ) was lower  
233 compared to that of propane ( $Le = 1.75 @ \phi = 0.8$ ) and butane ( $Le = 1.8 @ \phi = 0.8$ ) fuels; the main parts of  
234 LPG fuel. Consequently, due to the proximity of the NG Lewis number to unity, the turbulent burning  
235 velocity of NG flames was enhanced, and hence, the stability of the turbulent NG flames in comparison to  
236 LPG flames was improved [38-40]. Furthermore, the laminar flame speed of the NG/air mixture at lean  
237 equivalence ratio of  $\phi = 0.8$  was slightly higher compared to that of the LPG/air mixture [41, 42]. Therefore,  
238 the NG flames were more stable compared to the LPG flames.  
239

240 In addition, for  $L/D = 1$ , both the fuels with disk,  $d_s = 45$  mm yielded the minimum flame stability compared  
241 to the other  $L/D$  ratios. This behaviour could be linked to the lower mixing time ( $\tau_{mix}$ ) generated from the  
242 higher turbulence level associated with the large slit diameter [43]. The numerical analysis of the current  
243 burner using three-dimensional computational fluid dynamics (CFD) modelling quantified the higher axial  
244 and radial turbulent intensities accompanied with disk,  $d_s = 45$  mm, compared to that of disk,  $d_s = 25$  mm  
245 [42]. Consequently, improper air/fuel mixing will be generated during this shorter mixing length,  $L$ , due to  
246 the insufficient time available for the mixing process. Subsequently, an incomplete partial premixed flame  
247 will be produced at the burner tube exit [44], in comparison to the other  $L/D$  ratios, which contained longer  
248 mixing lengths. Furthermore, when the mixing time of the fuel and air during the burner mixing length  
249 becomes shorter than the chemical reaction time ( $\tau_c > \tau_{mix}$ ), the combustion can no longer be sustained, and  
250 this will reduce the flame stability. In addition, for the high levels of turbulence intensities, the flame will  
251 be quenched quickly, due to the higher mixing rate (scalar dissipation rate), characterized by the small  
252 length scale of the turbulence, in comparison to the smaller thickness ( $\delta$ ) of the laminar flame reaction-  
253 diffusion zone [45, 46].  
254

255 As the degree of partial premixing was increased to  $L/D = 2$  and  $3$ , the flame stability was increased for all  
256 of the cases, except the case of the NG/air mixture with  $d_s = 25$  mm, where the flame stability was gradually  
257 reduced. For both partially premixing ratios of  $L/D = 2$  and  $3$ , the LPG/air mixture with  $d_s = 45$  mm  
258 consistently had the minimum flame stability. The maximum flame stability was achieved at  $L/D = 3$  for  
259 LPG with disk,  $d_s = 25$  mm and NG with disk,  $d_s = 45$  mm. This could be attributed to the multi-reaction  
260 zones structure associated with a non-homogeneous mixture, which include lean, rich and diffusion [47].

261 Once these zones interacted, the likelihood of the triple flame structure formation increased, resulting in  
 262 higher flame stability [48, 49]. Regarding the flame images, all of the cases exhibited stable flames with a  
 263 blue colour, except LPG, ds = 45 mm, which yielded a lower stability with a small blue region near the flame  
 264 base followed by bright yellow flame with high luminosity.  
 265

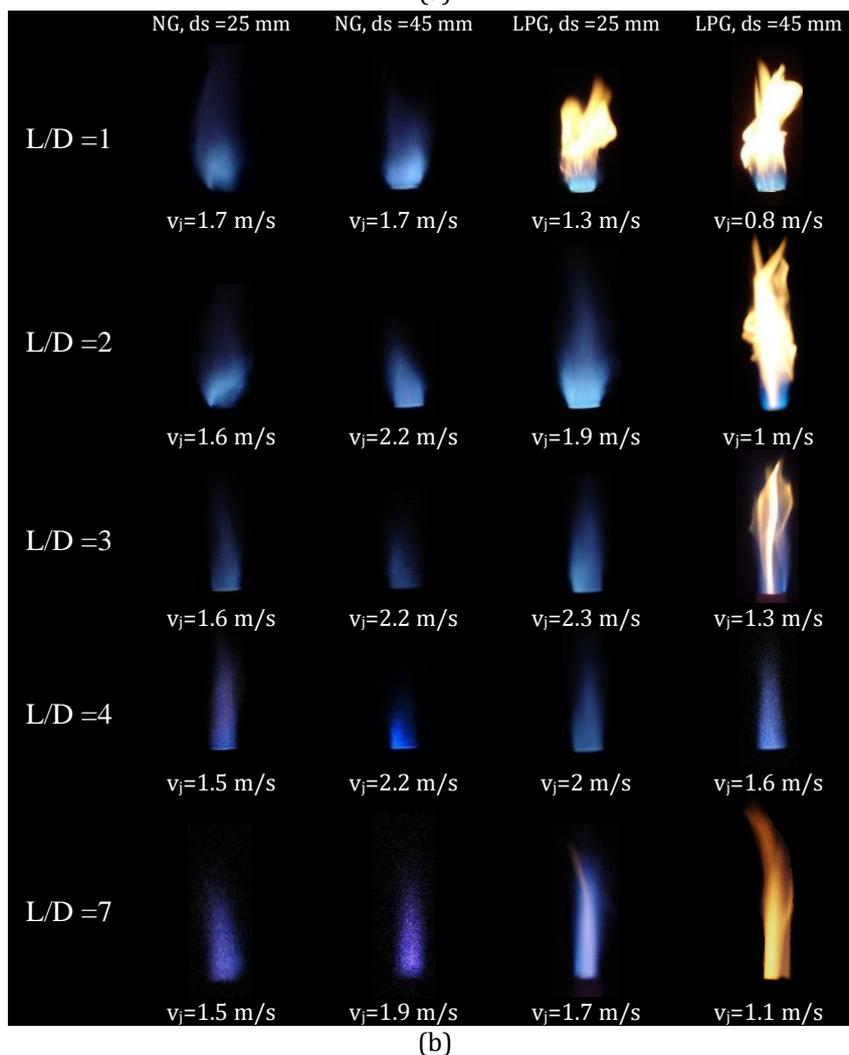
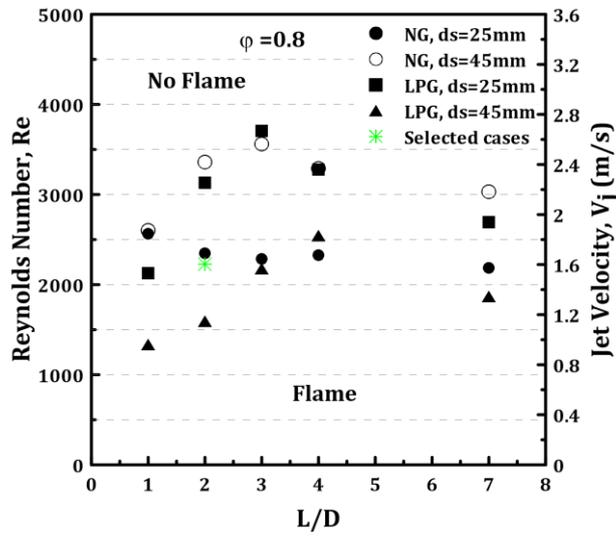


Figure 4. Impact of changing the disk slit diameter, fuel type and the level of partial premixed on (a) stability curves and (b) flame appearance of partially premixed flames.

266 However, with further increase of the degree of partial premixing to  $L/D = 4$ , the flame stability started to  
267 decrease for the NG/air mixture with  $d_s = 45$  mm, and the LPG/air mixture with  $d_s = 25$  mm, whilst the  
268 flame stability started to increase for the NG/air mixture with  $d_s = 25$  mm, and the LPG/air mixture with  
269  $d_s = 45$  mm. The minimum flame stability for the NG/air mixture was produced with  $d_s = 25$  mm. In the  
270 most well-mixed case of partial premixed degree  $L/D = 7$ , it was noticed that the flame stability was reduced  
271 for all of the cases.

272  
273 **Figure 4 (a)** also demonstrated the evolution of the jet velocity (where the blowout occurred) as a function  
274 of the level of the partially premixed  $L/D$ . For disk,  $d_s = 25$  mm, the maximum jet velocity of  $V_j = 1.8$  m/s  
275 was observed for NG at  $L/D = 1$ , whilst for LPG, the maximum jet velocity of  $V_j \approx 2.6$  m/s was observed at  
276  $L/D = 3$ . For disk,  $d_s = 45$  mm, the maximum jet velocity of  $V_j = 2.6$  m/s was observed for NG at  $L/D = 3$   
277 whilst for LPG, the maximum jet velocity of  $V_j \approx 1.8$  m/s was observed at  $L/D = 4$ . This enhancement in  
278 flame stability for these non-homogenous mixtures is linked to the higher probability of finding near-  
279 stoichiometric mixtures of fuel and air burning in contact with the hot burnt gases from the burner. This  
280 results in additional heat release at the base of the turbulent jet flame and helps to stabilize it.

281  
282 The flame stability at a constant level of partially premixed of  $L/D = 2$  was further examined under different  
283 Reynolds numbers and equivalence ratios, as presented in **Figure 5 (a)**. Furthermore, qualitative  
284 measurements of flame characteristics, such as flame shape, height and colour, associated with each case,  
285 have been observed, as shown in **Figure 5 (b)**. Four rows of images, which represent a comparison between  
286 LPG and NG, for two disk slit diameters of  $d_s = 25$  mm and  $d_s = 45$  mm, at different equivalence ratios, are  
287 displayed. The blowout limit was determined by maintaining a constant mass flow rate of the fuel stream  
288 whilst increasing the mass flow rate of the air stream until the flame extinction happened. Four extinction  
289 curves were established for each disk slit diameter and each fuel type. For the NG/air mixtures, changing  
290 the turbulence generator disk slit diameter had a small effect on the flame stability, especially at very lean  
291 conditions, where their behaviours were closely matched. On contrast, the flame stability of the LPG/air  
292 mixture was more susceptible to the change of the turbulence generator disk slit diameter. For lean mixture  
293 conditions of  $\phi < 0.8$ , the LPG/air mixture with  $d_s = 25$  mm yielded the maximum flame stability followed  
294 by the NG/air mixtures with  $d_s = 45$  mm and  $25$  mm, respectively. The flame stability completely  
295 deteriorated for the LPG/air mixture with  $d_s = 45$ mm, over the whole equivalence ratio range. The higher  
296 stability of LPG at lean conditions could be contributed to its higher calorific value (energy content) than  
297 natural gas, with  $93.2$  MJ/m<sup>3</sup> vs  $38.7$  MJ/m<sup>3</sup> [50], and thus, its higher heat release rate. The primary effect  
298 of an increase in the heat released by the flame is to increase the flame speed, and consequently, a small  
299 amount of LPG will produce a higher energy flame as compared to an equivalent amount of NG [51, 52]. A  
300 slightly higher flame stability was observed for the NG/air mixture, for the disk slit diameter of  $d_s = 25$  mm,  
301 as compared to disk slit diameter,  $d_s = 45$  mm, for lean conditions ( $\phi < 0.6$ ). This was due to the high  
302 susceptibility of the combustion systems operating at lean conditions to the high turbulence accompanied  
303 with  $d_s = 45$  mm, which promoted lower flame stability induced by local flame extinction [53].  
304 Consequently, this resulted in lower thermal diffusivity compared to the mass diffusivity and hence the rate  
305 of heat transfer could not keep pace with the rate of mass transfer, resulting in the flame becoming  
306 quenched.

307  
308 For equivalence ratios of  $\phi \geq 0.8$ , the NG/air mixture with  $d_s = 45$  mm demonstrated the maximum flame  
309 stability followed by the LPG/air mixture with  $d_s = 25$  mm, and the NG/air mixture with  $d_s = 25$  mm. A  
310 significant difference in the flame stability for the NG/air mixture with  $d_s = 45$  mm was noticed at the  
311 equivalence ratios of  $\phi = 0.8$  and  $0.9$ , as compared to that observed with  $d_s = 25$  mm. The high turbulence  
312 level associated with the large disk  $d_s = 45$  mm, resulted in an increase in the entrainment of the hot product  
313 gas and flame radicals towards incoming reactants, elevating the chemical reaction rate and hence the stabilization  
314 of the flame [54, 55]. LPG with  $d_s = 45$  mm, consistently had the minimum burner stability.

315  
316 Regarding the flame appearance, it was noticed for the NG/air mixtures, that the flame is more stable for  
317 both the disks, with a blue colour. In contrast, LPG with  $d_s = 45$  mm, yielded a completely diffusive flame  
318 with a bright yellow colour, without blue coloured flame near its base at very lean mixtures. As the  
319 equivalence ratio increased to rich conditions, the flame colour became blue. Likewise, the flame images  
320 reflected the higher stability of the flame associated with LPG,  $d_s = 25$  mm, for lean conditions, with a longer  
321 blue coloured flame near to the base of the flame with a small yellow coloured portion at the top of the  
322 flame. Additionally, for stoichiometric and rich conditions, the flame became more stable, with a blue colour.

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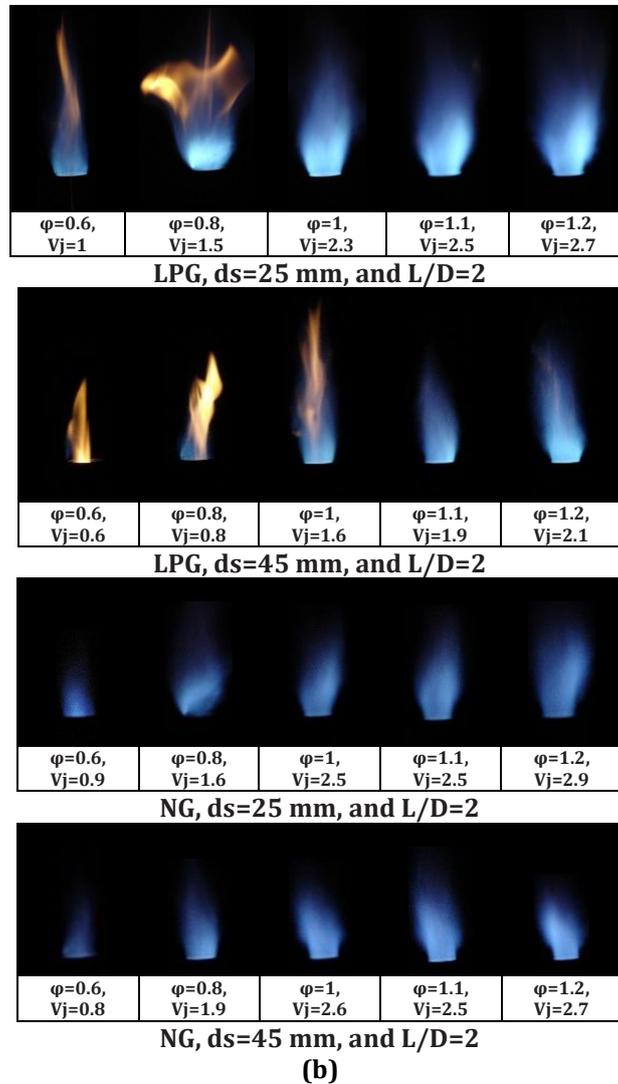
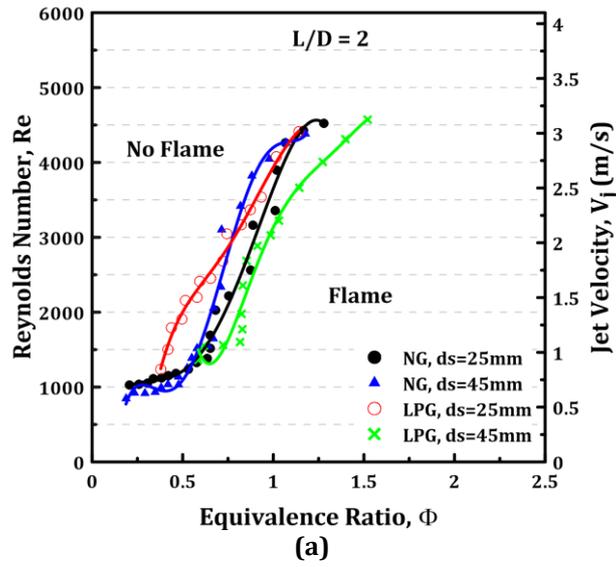


Figure 5. Impact of changing the disk slit diameter and fuel type on (a) stability curves (b) flame appearance of partially premixed flames at constant level of partial premixing, at  $L/D = 2$ .

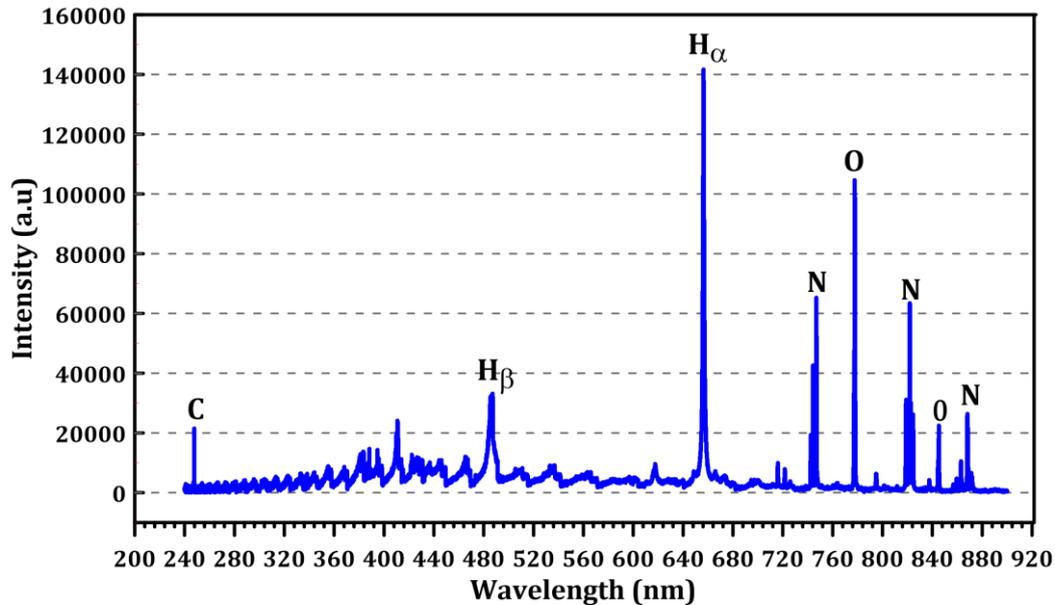
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### 3.2. LIBS spectra lines and calibration Lines

328 **3.2.1. LIBS spectra**

329

330 For turbulence disk slit diameter of  $d_s = 25\text{mm}$ , the break down LIBS spectrum, in the region between 240  
331 and 900 nm was measured for the lean NG/air mixture of  $\varphi = 0.8$  and jet velocity of  $V_j = 1.6\text{ m/s}$ , as shown  
332 in Figure 6. The incident laser energy was maintained constant at 100 mJ for all measurements, and the  
333 presented spectrum corresponded to an average of 50 laser shots. A broad band Echelle spectrometer was  
334 employed to collect the emission signal and the most common spectral atomic lines highlighted in the  
335 spectrum were C (I)-247.8 nm,  $H\alpha$  (I) - 656.4 nm, N (I)-747.2 nm and O (I)- 777.5 nm. Moreover, the N(I)  
336 atomic line consisted of three peaks at 742.5, 744.5, and 746.8 nm.  
337



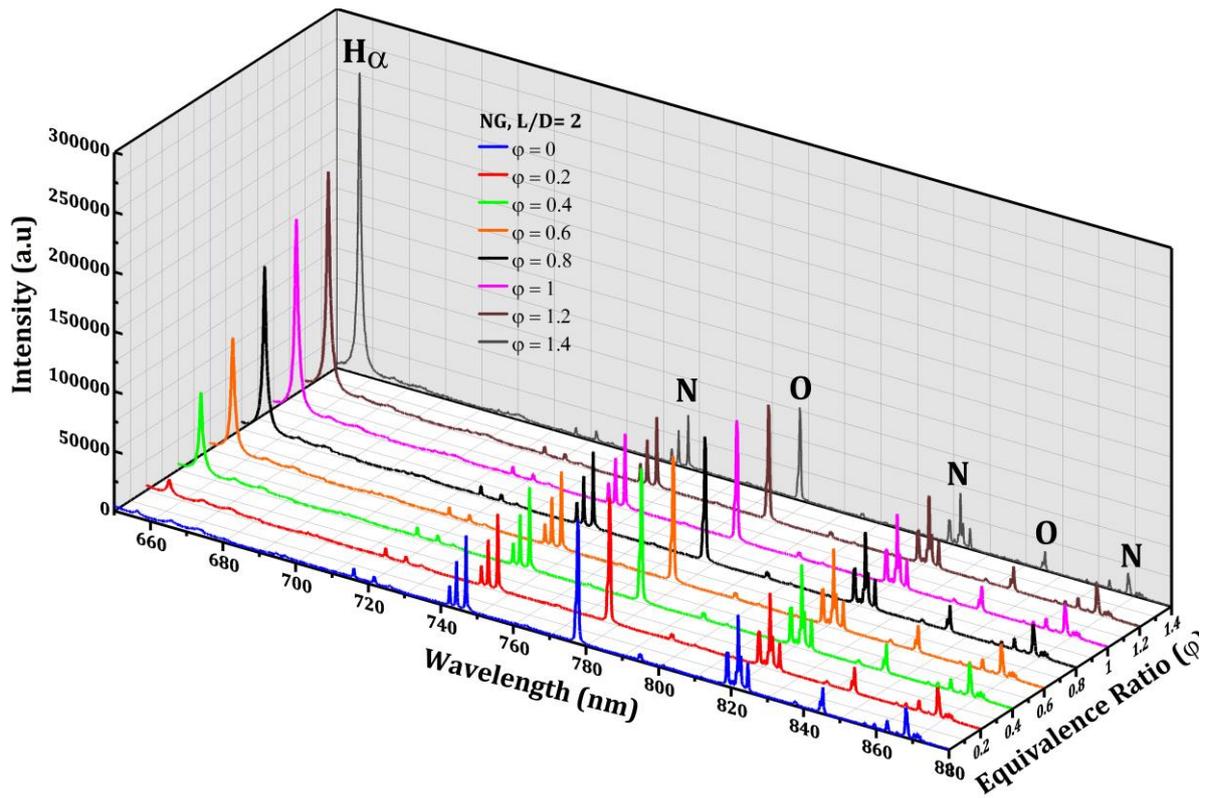
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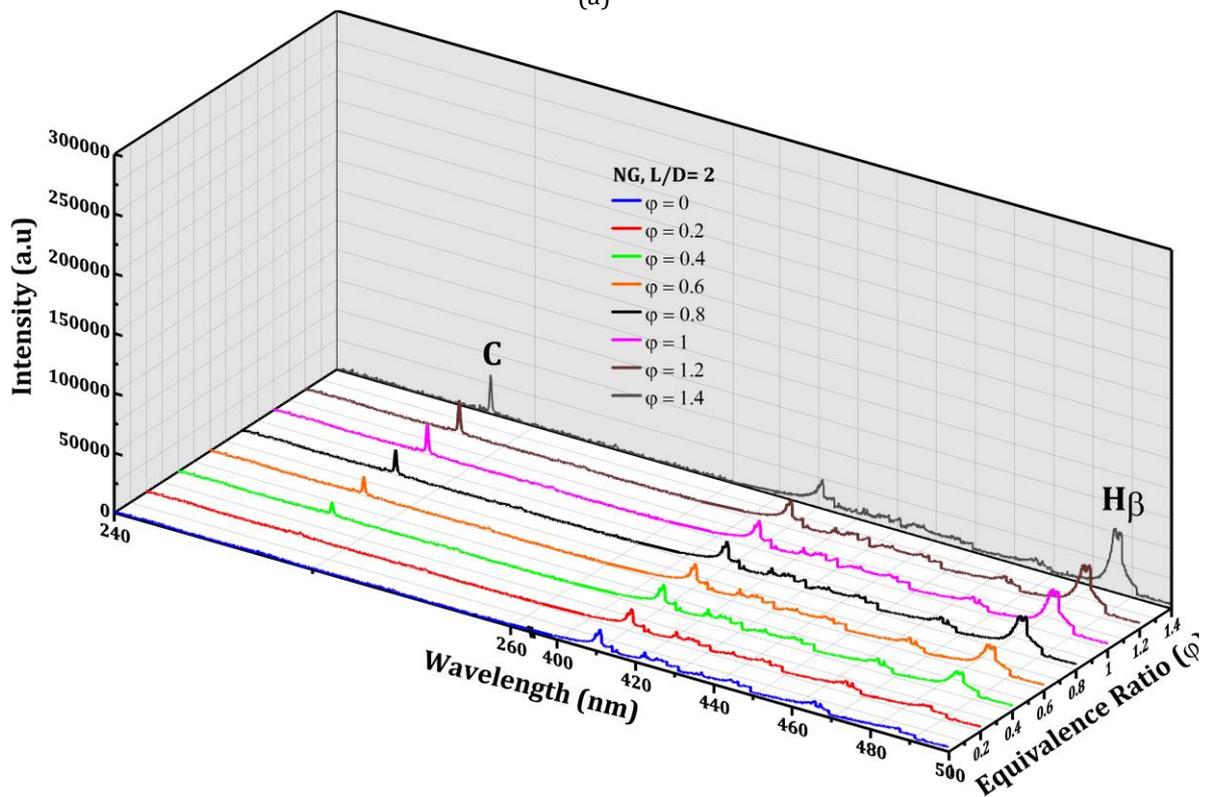
340 **Figure.6.** NG/air mixture typical break down LIBS spectrum in the region between 240 and 900 nm at an  
341 equivalence ratio of  $\varphi = 0.8$ .

342

343 The quantitative analysis of the local equivalence ratio measurements by the LIBS technique could be  
344 fulfilled by establishing a linear relationship between the value of the emission lines intensities and the  
345 equivalence ratio of a well premixed mixture. To ensure confidence regarding the high mixture  
346 homogeneity, a long-distance pipe with an approximate length of 200 times the pipe diameter was selected  
347 for the fuel-air mixing process, to create a perfectly homogeneous mixture. For the calibration purpose, a  
348 wide range of equivalence ratios, including eight sets of  $\varphi = 0, 0.2, 0.4, 0.6, 0.6, 0.8, 1$  and  $1.4$  were selected  
349 to evaluate the emission spectral line intensities of O (I),  $H\alpha$  (I), C (I), and N (I), for each set. The statistical  
350 analysis of the emission spectrum was conducted by using the GRAMS/AI V.8.0 Spectroscopy software  
351 package. The predominant atomic lines of C (I)-247.8 nm,  $H\alpha$  (I) - 656.4 nm, N (I)-747.2 nm and O (I) - 777.5  
352 nm for each equivalence ratio are presented in Figure 7. Based on the 50 single shot measurements carried  
353 out at each set, the calculated standard deviation of the predominant spectral line emission intensities was  
354 altered between 5-12%. The spectrum lines were captured with a 0.02 nm spectral resolution by using an  
355 ICCD camera attached to an Echelle spectrometer. Due to the air compositions which include 78.09%  
356 nitrogen, 20.95% oxygen, 0.93% argon, and 0.04% carbon dioxide, the carbon emission spectral line C (I)  
357 was noticed at an equivalence ratio of  $\varphi = 0$ . The increase of the equivalence ratio was associated with an  
358 increase in the intensity of C and H and a decrease in the intensity of O and N.



(a)



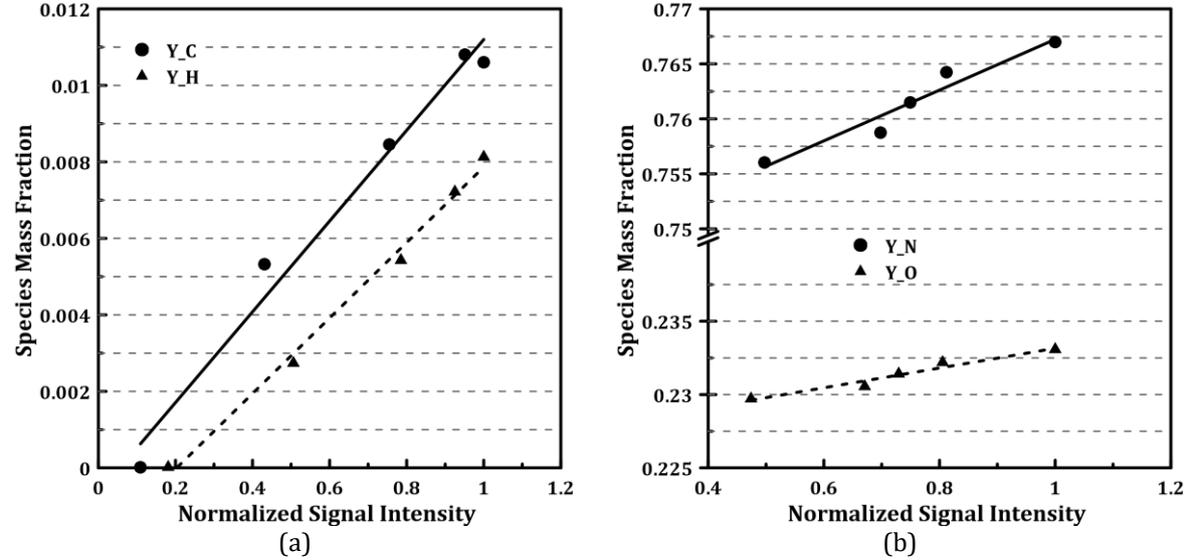
(b)

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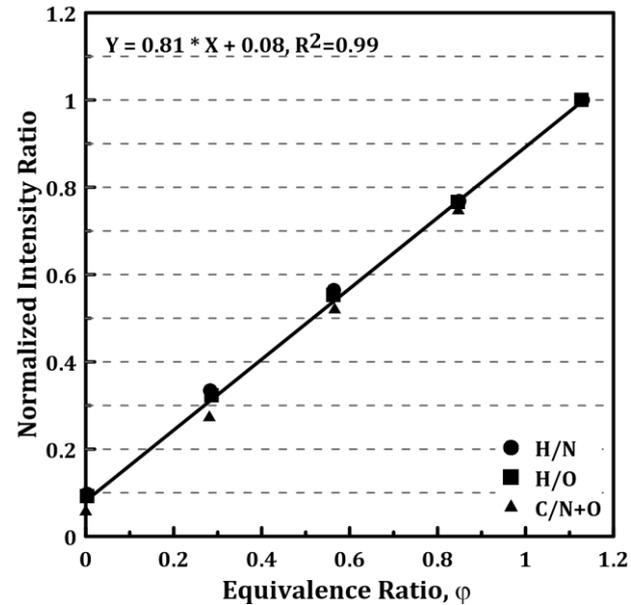
Figure 7. The LIBS spectra of C (I), H (I), N (I) and O (I) elements for a series of different equivalence ratios at  $\phi = 0, 0.2, 0.4, 0.6, 0.8, 1, 1.2$  and  $1.4$  for the NG/air mixture in the region between (a) 650-880 nm, and (b) 240-500 nm.

364 **3.2.2. Calibration lines**

365 From the spectrum analysis implemented in the aforementioned section, the elemental mass fractions  $Y_C$ ,  
 366  $Y_H$ ,  $Y_N$  and  $Y_O$ , were calculated and presented against the signal intensity as a linear relationship in [Figure](#)  
 367 [8](#). Due to the high precision of using the integral method of the area under each spectral line [[25](#), [56](#)], the  
 368 mass fraction of each emission line was defined by the ratio between the integration area under the peak  
 369 of this line and the total integration area under the peaks of all of the elemental spectral lines. The  
 370 normalized signal intensity was obtained by dividing the elemental signal intensity by the maximum  
 371 intensity of each element. The high linearity between the LIBS signal intensity and the elemental mass  
 372 fraction shows the high fidelity of the LIBS system for use as a measuring tool for equivalence ratio  
 373 quantitative measurements. The deviation of carbon and hydrogen elements from linearity at lower  
 374 concentrations could be contributed to the laser shot-to-shot fluctuation.  
 375



376 **Figure.8.** The elemental mass fractions (a)  $Y_C$  and  $Y_H$ , and (b)  $Y_N$  and  $Y_O$ , against the normalized signal  
 377 intensity.  
 378



379 **Figure.9.** Correlation between the elemental intensity ratio of (a) H/N, (b) H/O and (c) C/N+O, and the  
 380 equivalence ratio for the premixed NG/air mixture.  
 381  
 382

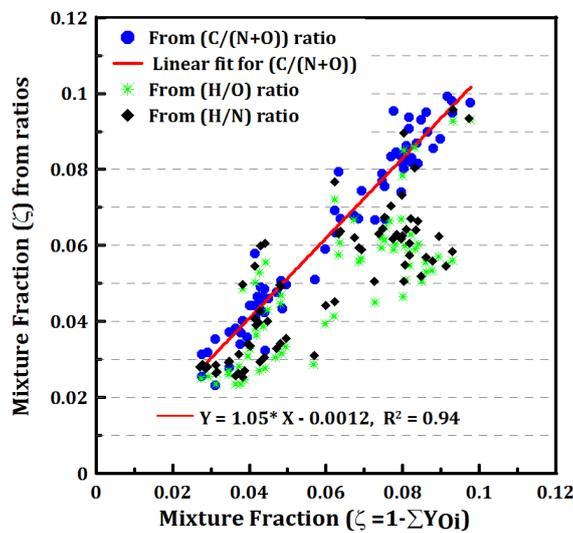
383 The C/(N+O), H/O and H/N intensity ratios were reported as a function of the equivalence ratio for the  
 384 NG/air mixtures, as shown in [Figure 9](#). The value of each intensity ratio was normalized to the maximum  
 385 intensity associated with this ratio. Moreover, the three ratios corresponded linearly to the equivalence

386 ratio of the premixed NG/air mixture. This calibration line will be essential for local equivalence ratio  
 387 measurements. The calibration procedure was accomplished under real temperature and pressure  
 388 conditions, which is directly related to the behaviour of the flames.  
 389

390 Two methods were utilized to evaluate the mixture fraction ( $\xi$ ); in the first method,  $\xi$  was calculated by  
 391 using the intensity ratios of C/(N+O), H/N and H/O, whilst the second method identified  $\xi$  based on the  
 392 obtained elemental mass fraction values, which are presented in Figure 8, and substituted it into Eq. (1).  
 393 Subsequently, a relationship between the two methods is presented in Figure 10. Over the entire range of  
 394 the mixture fraction measurements, the data showed good agreement, especially with the values  
 395 determined from the ratio C/(N+O). The intensity ratios of H<sub>656.3</sub>/O<sub>777.4</sub> and H<sub>656.3</sub>/N<sub>746.5</sub> yielded good  
 396 agreement with the  $\xi$  calculated from Eq. (2), at mixture fractions  $\xi = 0.03-0.05$  and for  $\xi = 0.07-0.09$ .  
 397 Consequently, both methods could be employed for mixture fraction quantitative measurements.

$$\xi = 1 - \sum y_{oi} \tag{Eq (1)}$$

398 where  $y_{oi}$  are the oxidant elements' mass fractions. Thus,  $\xi$  for the fuel stream will be 1, and for the oxidizer  
 399 stream, it will be 0.  
 400

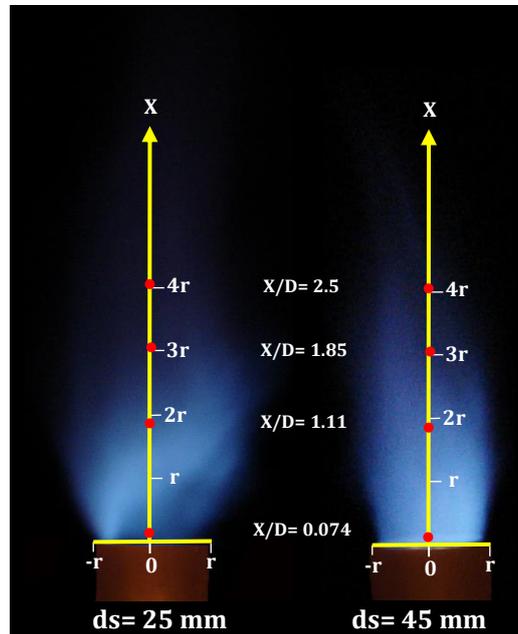


401  
 402  
 403 **Figure.10.** Comparison of the mixture fraction calculation for a partially premixed flame at equivalence  
 404 ratios of 0.8 and jet velocity of 1.6 m/s, using the three ratios of (C/(N+O)), (H/O) and (H/N), represented  
 405 by the y-axis, and that calculated from Eq. (2) based on the elemental mass fractions represented by the x-  
 406 axis.  
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424 **3.3. Mass Fraction Measurements**

425

426 The flame appearance and the location of the measurement axial positions (red dots) of the lean partially  
 427 premixed flame at the equivalence ratio,  $\phi = 0.8$ , with two disk slit diameters, for the NG/air mixture, is  
 428 shown in Figure 11.



429

430 **Figure.11.** The flame appearance and the location of the measurement axial positions (red dots) of the lean  
 431 partially premixed flame at the equivalence ratio,  $\phi = 0.8$  and  $V_j = 1.6$  m/s, with two disk slit diameters, for  
 432 the NG/air mixture.

433

434 **Figure 12** shows the mass fraction radial distribution of different elements including O, N, H and C with the  
 435 two disk slit diameters of  $ds = 25$  mm and  $ds = 45$  mm, at further distances from the burner rim. Around  
 436 the burner axis, a perfectly symmetrical distribution of the mass fraction occurred. A perfectly flat shaped  
 437 distribution occurred with the large slit diameter of  $ds = 45$  mm, whilst a triangular shaped  
 438 distribution occurred with a lower slit diameter of  $ds = 25$  mm. In comparison to the lower disk slit diameter of  $ds = 25$   
 439 mm, the larger disk slit diameter of  $ds = 45$  mm had a lower mass fraction distribution for elements H and  
 440 C, and a higher oxidant elemental mass fraction of N and O over the radial region of  $-0.5 \leq r/R \leq 0.5$ . For  
 441 disk,  $ds = 45$  mm, the reduction in C and H mass fractions at  $X/D = 0.074$  was approximately 8%, and as the  
 442 distance from the burner rim further increased to  $X/D = 2.5$ , the reduction in C and H mass fractions  
 443 increased up to 30% in comparison to those observed with the disk,  $ds = 25$  mm. This can be understood  
 444 by referring to the numerical analysis of the current burner, which showed that the large disk,  $ds = 45$  mm,  
 445 was associated with higher turbulence intensity, and subsequently, the mixing layer during the burner  
 446 mixing length,  $L$ , will be changed [43]. This higher intensity will be associated with a large rate of strain,  
 447 which reduced the annulus fuel stream, to entrain more into the air stream and the rate of molecular  
 448 diffusion will be reduced, resulting in higher  $Y_N$  &  $Y_O$  and lower  $Y_C$ , &  $Y_H$  [57-59].

449

450 The elemental mass fraction of H and C were reduced for both disks, as the distance from the burner rim  
 451 increased further, due to the increased time available for the surrounding air to penetrate into the partially  
 452 premixed flame [26]. It was noticed that the elemental mass fraction of H and C were reduced for both the  
 453 disks as the distance from the burner rim further increased due to the increased time available for the  
 454 surrounding air to penetrate deeper into the partially premixed flame. Furthermore, at the edge of the  
 455 burner the values of the elemental mass fraction of O and N were very close to that components of  
 456 atmospheric air, and moving toward the burner centerline, these values were reduced. This could be linked  
 457 to the shear layer generated due to the diffusion between the air and fuel.

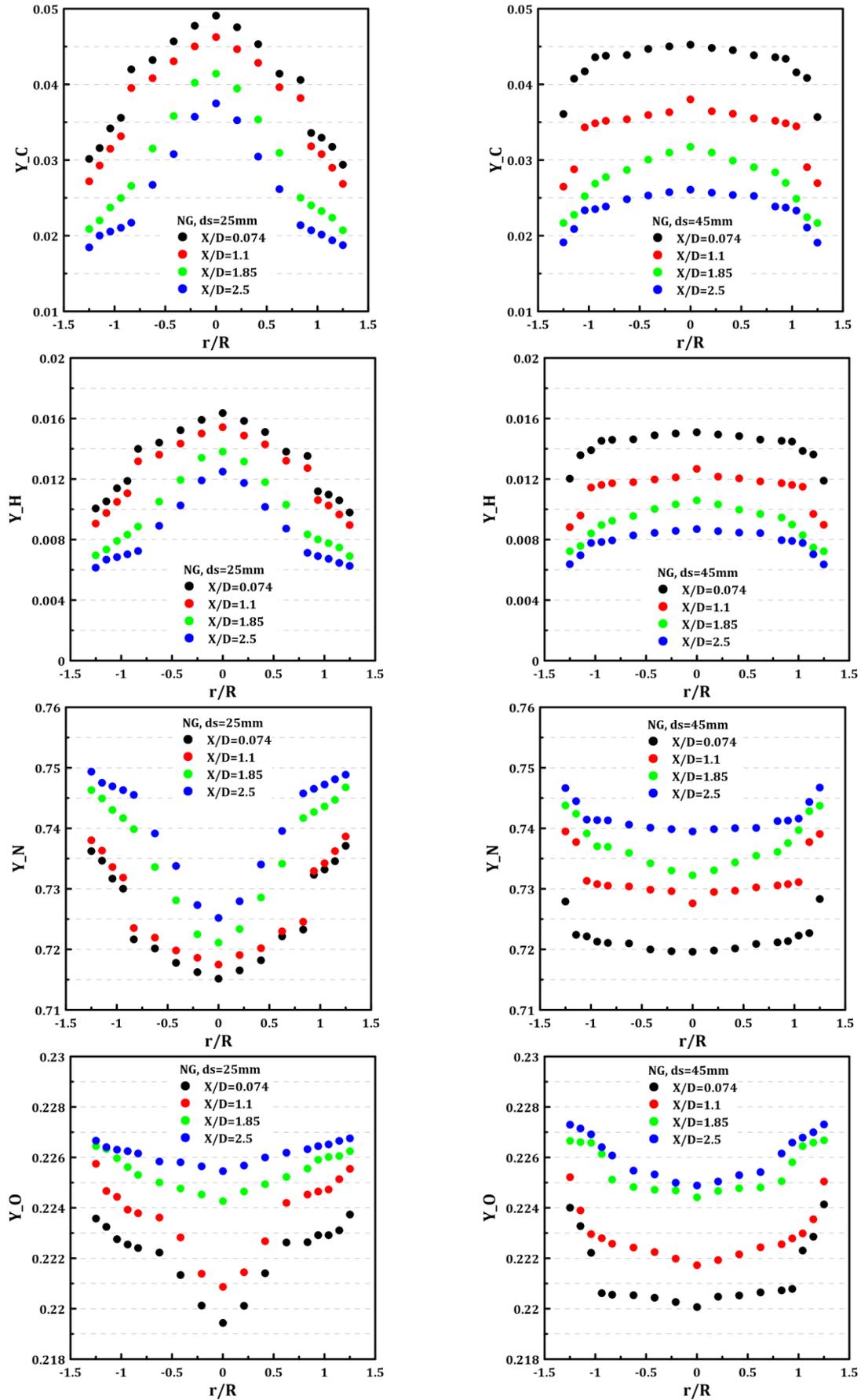


Figure.12. Effect of changing the disk slit diameter on the elemental mass fraction distributions for the lean partially premixed flame of  $\phi = 0.8$  at different axial positions for the NG/air mixture.

### 3.4. Mixture Fraction Measurements

Based on the calibration curves shown in Figure 9, the local equivalence ratio could be identified for each measured point according to any of the three intensity ratios C/(N+O), H/N and H/O. The local equivalence ratio was calculated as an average of 50 laser shots. Then the mixture fraction  $\xi$  can be either calculated based on the obtained elemental mass fractions values presented in Figure 8 and substituted in Eq. (2), or by using the local equivalence ratio determined from the linear calibration trend and substituting it into Eq. (3):

$$\xi = \sum y_{Fi} \quad (2)$$

where  $y_{Fi}$  are the fuel elements' mass fractions. Furthermore, the mixture fraction,  $\xi$  can be employed to evaluate the average equivalence ratio based on Eq. (3):

$$\xi = \frac{\varphi}{\varphi + \left(\frac{A}{F}\right)_{st}} \quad (3)$$

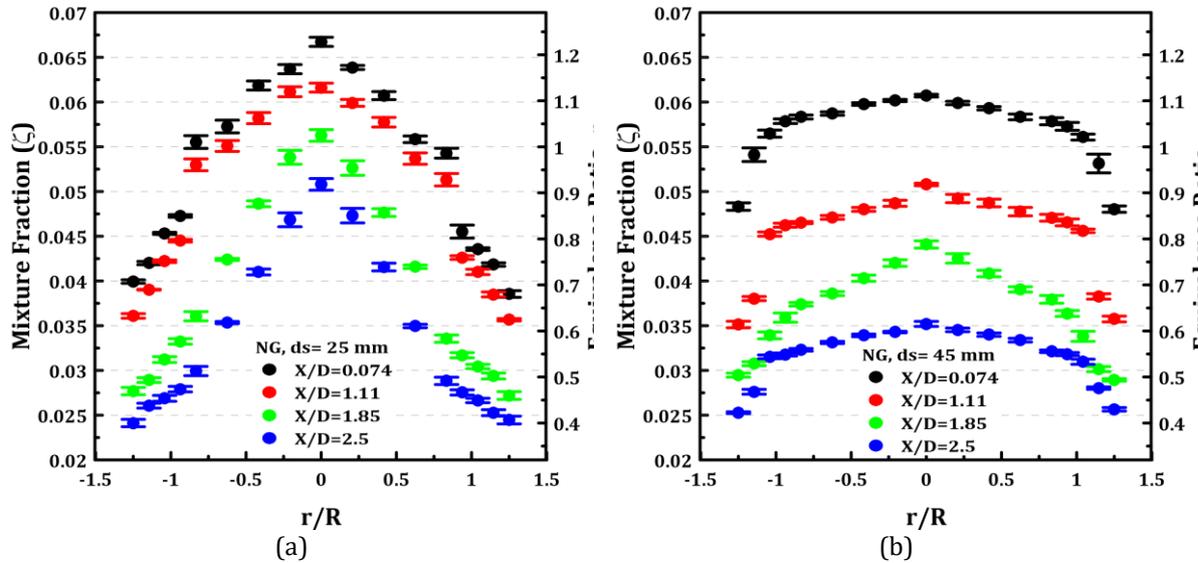
For the current NG/air flame the stoichiometric air-to-fuel ratio  $(A/F)_{st}$  was calculated as 17.167.

The impact of changing the disk slit diameter on the mean radial profile distribution of equivalence ratio or mixture fraction at different axial positions of  $X/D = 0.074, 1.11, 1.85$  and  $2.5$  are presented in Figure 13. All of the measurements were conducted at lean NG/air mixture conditions of  $\varphi = 0.8$ ,  $V_j = 1.6$  m/s and partially premixed degree of  $L/D = 2$ , to investigate the structure of the flame. The results demonstrated that the equivalence ratio distributions were significantly influenced by altering the disk slit diameter, due to variation of both the mean flow structure and the level of turbulence intensity associated with each disk [60].

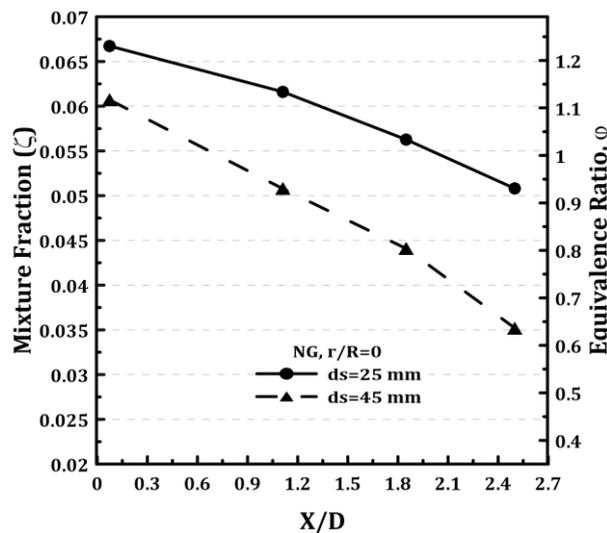
Figure 13 illustrates that around the burner axis, a perfectly symmetrical distribution of the mixture fraction,  $\xi$  profile was manifested, and the mixture fraction values peaked at the burner axis and rapidly decreased towards the periphery (air side), especially for lower disk slit diameter,  $ds = 25$  mm. This could be interpreted by referring to the numerical investigation of the turbulent intensity produced from the current burner at  $L/D = 2$  [43]. It was noticed that disk  $ds = 25$  mm had a faster decay rate of the turbulent intensity during the mixing length,  $L$ , in comparison to that of  $ds = 45$  mm. Consequently, a higher percentage of the fuel introduced through the annulus will be diffused towards the burner centerline for  $ds = 25$  mm during the mixing length,  $L$ . The higher level of intensity associated with the large disk,  $ds = 45$  mm, yielded eddies of sufficient strength and with a large rate of strain, which enhanced the entrainment of the annulus fuel to the air stream. As a result, a homogenous mixture fraction distribution will be produced and this was consistent with the results of Meares and Masri [61], where the fuel was introduced by the same way.

As shown in Figure 13, the smaller turbulence generator disk slit diameter of  $ds = 25$  mm consistently encompassed a wide range of equivalence ratios distributions in comparison to that of  $ds = 45$  mm. At an axial distance of  $X/D = 0.074$ , the radial distribution of  $\varphi$  for disk  $ds = 25$  mm was varied from very lean condition of  $\varphi = 0.67$  to very rich conditions of  $\varphi = 1.25$ , whilst for the disk  $ds = 45$  mm, the radial local equivalence ratio profiles were varied from a slightly lean condition of  $\varphi = 0.86$  to a slightly rich condition of  $\varphi = 1.1$ . As the axial distance from the burner rim further increased, the radial distribution of  $\varphi$  became narrower and the flames were naturally anchored to the burner lips and they took a conical shape, especially at an axial distance of  $X/D = 2.5$  for  $ds = 25$  mm [62]. Furthermore, the disk slit diameter,  $ds = 45$  mm, had a perfectly flat local equivalence ratio distribution for axial distances of  $X/D = 0.074$  and  $1.11$ , within the burner wall boundary. Also, the created flammable region for disk,  $ds = 25$  mm, was decreased from rich condition around  $\varphi = 1.25$  on the jet axis to stoichiometric conditions at  $r/R = 0.5$  and then to lean conditions, while moving radially further toward the air side. For the disk,  $ds = 45$  mm, a rich homogeneous mixture of  $\varphi=1.1$  was radially distributed over the burner wall boundary and then started to decrease into stoichiometric and lean conditions at the periphery (air side).

509 The high turbulence level associated with the large disk,  $ds = 45$  mm, resulted in an increase in the  
 510 entrainment of the hot product gas and flame radicals towards incoming reactants, elevating the chemical reaction  
 511 rate, and hence, it helped to stabilize the flame [63-65]. Furthermore, this kind of mixing between the products  
 512 and reactants diluted the mixture fraction of disk,  $ds = 45$  mm, as compared to that of disk,  $ds = 25$  mm. The  
 513 reduction in mixture fraction values at distances further from the burner rim can be mainly attributed to the  
 514 enough time available for the surrounding air to penetrate deeper into the partially premixed flame  
 515 [26]. Moreover, the mixture fraction flat distribution profiles highlight the ability of the current burner  
 516 configuration to generate highly stable partially premixed flames. In addition, previous studies [8, 66]  
 517 showed that the flame speed is directly proportional to the mixture fraction gradient and subsequently the  
 518 flame front curvature. Consequently, the non-uniformity in the  $\xi$  distribution increased the flame front  
 519 curvature and decreased the rate of heat transfer from the flame front, resulting in a lower preheating of  
 520 the unburned gas layers, and hence, a lower flame propagation speed will be produced [8].  
 521



522 **Figure.13.** Impact of changing the disk slit diameter (a)  $ds = 25$  mm and (b)  $ds = 45$  mm, on the mean radial  
 523 profiles of equivalence ratio or mixture fraction distributions for the NG/air mixture at  $\phi = 0.8$ ,  $V_j = 1.6$  m/s  
 524 and  $L/D = 2$  for certain axial distances.  
 525

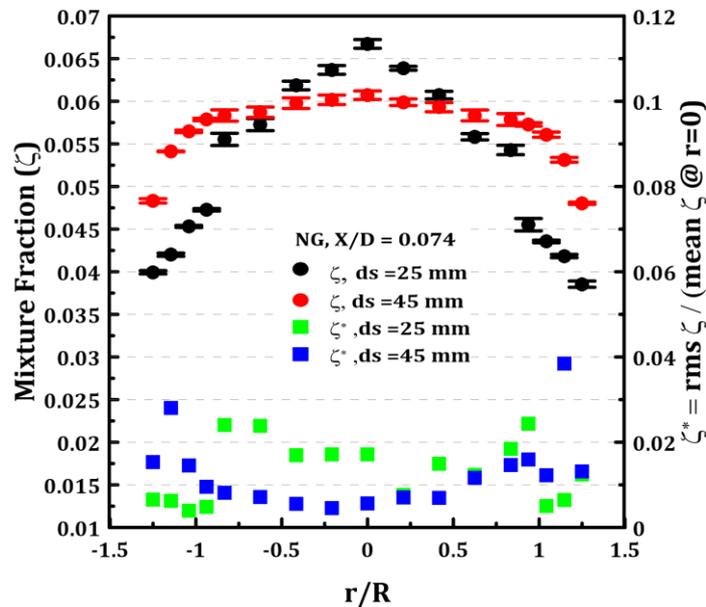


526 **Figure.14.** Variation of the equivalence ratio at different axial positions from the burner tip along the burner  
 527 centerline with different disk slit diameters of  $ds = 25$  mm and  $ds = 45$  mm, for the NG/air mixture at  $\phi =$   
 528  $0.8$ ,  $V_j = 1.6$  m/s and  $L/D = 2$ .  
 529  
 530

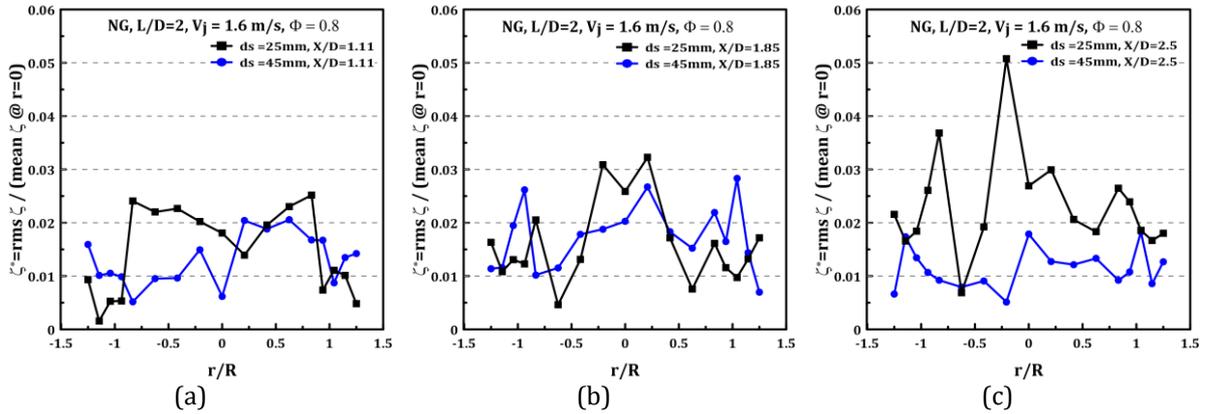
531 **Figure 14** highlighted the reduction of the equivalence ratio with the increase of the axial distances along  
 532 the burner centerline for different disk slit diameters. Consistently, disk,  $ds = 25$  mm had a higher

533 equivalence ratio at all the axial distances in comparison to disk,  $d_s = 45$  mm. This influence was mainly  
 534 linked to the enhancement of the surrounding air entrainment due to the higher level of turbulence  
 535 intensity associated with the large disk,  $d_s = 45$  mm. As the axial distance above the burner tip increased  
 536 from 0.074 to 2.5, the equivalence ratio was reduced for both the  $d_s = 25$  mm and  $d_s = 45$  mm disks by  
 537 approximately 25% and 43%, respectively. In addition, at an axial distance of  $X/D = 0.074$ , the equivalence  
 538 ratio for disk,  $d_s = 25$  mm, was higher than that of disk,  $d_s = 45$  mm, with approximately 9.6%. As the axial  
 539 distance from the burner tip increased to  $X/D = 2.5$ , the difference in the equivalence ratio between disk,  
 540  $d_s = 25$  mm and disk,  $d_s = 45$  mm, increased up to approximately 32%.

541  
 542 The fluctuation in mixture fraction were calculated as a ratio between the root mean square of the mixture  
 543 fraction fluctuations and the average of the mixture fraction values along the burner centerline. Both the  
 544 mean and fluctuating mixture fraction profiles ( $\xi$  and  $\xi^*$ , respectively) are presented in Figure 15 for an  
 545 axial distance of  $X/D = 0.074$ . For the lower disk slit diameter,  $d_s = 25$  mm, and lean mixture of  $\phi = 0.8$ ,  
 546 higher fluctuations occurred within the burner wall boundary compared to those observed with disk,  $d_s =$   
 547 45 mm. In contrast, outside the burner boundary disk,  $d_s = 25$  mm yielded lower fluctuations compared to  
 548 disk,  $d_s = 45$  mm. At  $X/D = 0.074$  and  $-1 \leq r/R \leq 1$ , the peak fluctuation for disk,  $d_s = 25$  mm, was  
 549 approximately 0.028, whilst for disk,  $d_s = 45$  mm, it was approximately 0.017. Moreover, across the burner  
 550 region of  $-0.5 \leq r/R \leq 0.5$ , the mixture fraction fluctuation associated with the disk,  $d_s = 45$  mm, was nearly  
 551 fixed around 0.008, and lower compared to that of the lower disk,  $d_s = 25$  mm, with approximately 0.019.  
 552 Figure 16 shows the fluctuating mixture fraction profiles  $\xi^*$  for the NG/air mixture at  $\phi = 0.8$  and  $L/D = 2$ ,  
 553 at further axial positions from the burner rim. The mixture fraction fluctuation profiles for disk,  $d_s = 45$   
 554 mm, were consistently lower than that of  $d_s = 25$  mm, for most of the radial distances  $r/R$ . The maximum  
 555 fluctuation was noticed for disk,  $d_s = 25$  mm at an axial distance of  $X/D = 2.5$  with  $\xi^* = 0.05$ . At an axial  
 556 distance of  $X/D = 1.11$ , the fluctuation trends for disk,  $d_s = 25$  mm, was slightly higher than that of the disk,  
 557  $d_s = 45$  mm. While at axial distance of  $X/D = 1.85$ , the fluctuation trends for both disks were close to each  
 558 other.  
 559



560  
 561 Figure.15. Impact of changing the disk slit diameter on both the mean and fluctuating mixture fraction  
 562 profiles for the NG/air mixture at  $\phi = 0.8$  and  $L/D = 2$  for the axial distance of  $X/D = 0.074$ .  
 563



564 **Figure.16.** Impact of changing the disk slit diameter on the fluctuation of the mixture fraction profiles for  
 565 NG/air mixtures at  $\phi = 0.8$  and  $L/D = 2$  for axial distances of (a)  $X/D = 1.1$ , (a)  $X/D = 1.85$  and (a)  $X/D = 2.5$ .

566  
 567 **Conclusions**

568  
 569 The current study was mainly focused towards the extension of the lean combustion limit by generating  
 570 higher turbulence levels or by using the partially stratified charge method. Likewise, the burner was  
 571 designed for improving the stability of lean flames, and consequently, it produces low emissions. In addition,  
 572 the LIBS technique was employed to characterize and quantify the impact of changing the disk slit diameter  
 573 on the distribution profiles of equivalence ratio or mixture fraction for NG/air partially premixed flame.  
 574 The current burner configuration stability was examined for a lean NG/air mixture at  $\phi = 0.8$  by changing  
 575 the disk slit diameters, the fuel used and the degree of partial premixing. The conclusions drawn from this  
 576 work are as follow:

- 577  
 578 (1) At the equivalence ratio of  $\phi = 0.8$  and for different levels of partially premixing, it was noticed that  
 579 changing the disk slit diameter has a great impact on the flame stability for both NG and LPG fuels.  
 580 Increasing the disk slit diameter from  $ds = 25$  mm to  $ds = 45$  mm resulted in a higher flame stability for the  
 581 NG/air mixture. In contrast, increasing the disk slit diameter for LPG/air mixtures reduced its flame  
 582 stability.  
 583  
 584 (2) Changing the level of partial premixing ( $L/D$ ) lead to an enhancement in the flame stability for both  
 585 fuels. However, the optimum  $L/D$  ratio where the maximum flame stability occurred varied based on which  
 586 fuel type and disk slit diameter was used.  $L/D = 1$  was the optimum ratio for NG with disk,  $ds = 25$  mm, at  
 587 which the maximum flame stability was achieved. The maximum flame stability was achieved at  $L/D = 3$   
 588 for LPG with disk,  $ds = 25$  mm, and for NG with disk,  $ds = 45$  mm. Finally, for LPG with disk,  $ds = 45$ mm,  $L/D$   
 589  $= 4$  was the optimum ratio at which the maximum flame stability occurred.  
 590  
 591 (3) Among all the cases, the NG/air mixture with  $ds = 45$  mm and  $\phi = 0.8$  demonstrated the maximum flame  
 592 stability, whilst the LPG/air mixture with  $ds = 45$  mm and  $\phi = 0.8$ , yielded the minimum flame stability over  
 593 different levels of partial premixing.  
 594  
 595 (4) At a constant level of partially premixing of  $L/D = 2$ , it was noticed that for equivalence ratios of  $\phi \geq 0.8$ ,  
 596 the NG/air mixture with  $ds = 45$  mm exhibited the maximum flame stability. Whilst for equivalence ratios  
 597 of  $\phi < 0.8$ , the LPG/air mixture with  $ds = 25$  mm yielded the maximum flame stability.  
 598  
 599 (5) The larger disk slit diameter,  $ds = 45$  mm, demonstrated almost zero mixture fraction gradients  
 600 distributions and lower fluctuation of the mixture fraction distributions within the burner wall boundary  
 601 in comparison to that of disk,  $ds = 25$  mm, for the NG/air mixture at  $\phi = 0.8$  and  $L/D = 2$ .  
 602  
 603 (6) Along the burner centerline disk,  $ds = 25$  mm consistently had a higher equivalence ratio at all of the  
 604 axial distances in comparison to disk,  $ds = 45$  mm. The equivalence ratio at axial distances of  $X/D = 0.074$   
 605 and  $X/D = 2.5$ , for disk,  $ds = 25$ mm, was higher than that of disk,  $ds = 45$ mm, with approximately 9.6% and  
 606 32%, respectively. As the axial distance above the burner tip increased from 0.074 to 2.5, the equivalence  
 607 ratio was reduced for both disks,  $ds = 25$ mm, and  $ds = 45$ mm, by approximately 25% and 43%, respectively.  
 608  
 609 (7) The mixture fraction fluctuation profiles associated with disk,  $ds = 45$ mm, were consistently lower than  
 that of  $ds = 25$ mm, for most of the radial distances  $r/R$ . Near the burner tip at  $X/D = 0.074$ , the peak

610 fluctuation for disk,  $d_s = 25\text{mm}$ , was approximately 0.028, whilst for disk,  $d_s = 45\text{ mm}$ , was approximately  
611 0.017. The maximum fluctuation was observed for disk,  $d_s = 25\text{mm}$ , at an axial distance of  $X/D = 2.5$  with  
612  $\xi^* = 0.05$ .

613

### 614 *Acknowledgement*

615

616 The authors would like to acknowledge the support from Dr Ivan Langella for his advice, support and  
617 positive feedback.

618

### 619 *References*

620

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