## Don't throw rocks from the side-lines: The Effect of "Wave Breakers" on the Magnetohydrodynamic Instability in Aluminum Reduction Cells

Pedcenko, A, Molokov, S & Bardet, B

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1	The effect of 'wave breakers' on the
2	magnetohydrodynamic instability in
3	aluminium reduction cells*
4	Alex Pedcenko <sup>*a</sup> , Sergei Molokov <sup>a</sup> , and Benoit Bardet <sup>b</sup>
5	<sup>a</sup> Coventry University, Priory Street, CV1 5FB, Coventry, UK
6	<sup>b</sup> Rio Tinto – LRF, rue Henri Sainte Claire Deville, CS 40114,
7	73302 St-Jean-de-Maurienne cedex, France
8	$\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ $
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#### Abstract 10

We report the results of the experiments on the suppression of the MHD 11 instability in a model of the aluminium reduction cells [1]. The idea behind 12 the study is to introduce obstacles in the liquid metal to suppress the propa-13 gation of the rolling-pad instability wave. As a result, in some configurations 14 with obstacles we detect lowering of the wave amplitude, reduction of its 15 propagation speed and rise of the main parameters' thresholds, responsible 16 for the instability onset. 17

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#### 18 1 Introduction

The effective control of magnetohydrodynamic (MHD) instabilities in alu-19 minium reduction cells is the problem of great importance. The process of 20 primary aluminium production (aluminium smelting) is based on the elec-21 trolytic reduction of the metallic aluminium from its high melting point oxide: 22 alumina (2345 K (2072°C)). In this technology, known as Hall-Héroult pro-23 cess, the alumina is dissolved in molten cryolite<sup>1</sup>, which lowers its melting 24 point and improves its electric conductivity. This solution is contained at 25 1233 K (960°C) in large (e.g.  $13 \times 4 \times 0.3$ m) rectangular cells – electrolytic 26 pots, with graphite top and bottom lining, serving as the anode and cath-27 ode electrodes respectively. High electric current of several hundreds kA is 28 then passed through the cell, and, as a result of the electrochemical reaction, 20 the liquid aluminium "pad" is formed under the cryolite, at the bottom of 30 the cell. The process is relatively expensive due to the amount of electricity 31 required for the reduction of each kilogramme of aluminium (11...14 kWh). 32 The main loss of energy is due to low electric conductivity of cryolite, so 33 reducing its thickness by every millimetre can result in substantial savings 34 worldwide. 35

Unfortunately, when the cryolite thickness<sup>2</sup> is reduced below a certain 36 threshold, such a binary system of two immiscible fluids with the vast dif-37 ference in their electrical conductivities and very small difference in densi-38 ties, becomes unstable owing to the electromagnetic body force. This force 39 appears due to the interaction of the horizontal component of the electric 40 current and vertical component of the background magnetic field, produced 41 by the bus bars supplying electricity to the cell. This interfacial instabil-42 ity, being magnetohydrodynamic in nature, is known to produce sloshing or 43 "rolling-pad" waves [4] at the interface between the cryolite and aluminium, 44 propagating along the perimeter of the cell in a rotating fashion. Such distur-45 bances of the interface can reduce effectiveness of the smelting process and 46 disrupt the normal operation of the cell or even the whole pot-line. Thus, 47 the control and suppression of unstable surface waves is one of the important 48 problems in aluminium smelting. 49

Since pioneering work by T. Sele [4], who identified the basic mechanism for the interface motion, many theoretical studies were devoted to the under-

 $<sup>^1 {\</sup>rm sodium}$  a luminium fluoride salt

<sup>&</sup>lt;sup>2</sup>known also as the anode to cathode distance, ACD

standing of the impact of different technological factors on the fluid motion 52 in the aluminium layer. Experimental investigation of the phenomenon, how-53 ever, is quite complicated due to the lack of safe and accessible experimental 54 modelling materials with the required physical properties. One of the possi-55 ble solutions proposed in [1] is to replace in the model the poorly conducting 56 cryolite with an array of  $30 \times 30$ ,  $\oslash 2$ mm-thin, vertical stainless steel elec-57 trodes, which when immersed in the liquid metal, supply the electric current 58 to its free surface and do not obstruct its vertical motion. Because the ef-59 fective electric resistance of such an array of thin conductors is about 100 60 times higher than that of liquid metal, the tilt of the interface will result in 61 the redistribution of the electric current between all parallel electrodes. This 62 creates a horizontal component of the current  $j_{\perp}$  in the better conducting 63 liquid metal, as the current needs to spread there before entering less con-64 ductive bottom of the cell. Externally imposed vertical magnetic field B of a 65 sufficient strength (up to 100 mT) triggers a horizontal motion of the liquid 66 metal due to the appearance of the electromagnetic Lorentz force  $\vec{i} \wedge \vec{B}$ , even-67 tually resulting in the rolling surface wave with a growing amplitude. Such a 68 physical model does not pretend to replicate the entirety of electrodynamic 69 processes occurring in the real cell, but it mimics the basic principle of the 70 Sele-type MHD instability and thus is dynamically similar to the instability 71 in real cells. The advantages of this experimental model have been discussed 72 in 1. The present report is an extension of the previous experimental study 73 published in [1] and modelling work presented in [2]. 74

### 75 2 Presentation of the problem

One of the possible ways to suppress the sloshing motion of a fluid is to introduce obstacles (i.e. "wave breakers"). For example, partitioning walls or baffles are used in tankers to suppress a surge or sloshing of liquids during transportation.

Song *et al.* in [5] report some slowing down of the liquid metal using "cathode with protrusions" in both numerical and industrial trials of . Dupuis and Bojarevics ([6],[7],[8]) report that the overall damping effect is not that significant, but all agree that such protrusions can increase the horizontal current in the liquid metal, which is responsible for the instability onset. It seems that the balance between these two effects will determine the success or otherwise of such a cathode construction. In our study we use non-conductive <sup>87</sup> "protrusions", which have no influence on the current distribution in the
<sup>88</sup> liquid metal, and their role is purely hydrodynamic.

The experimental cell (Fig.2) used in this work has the same construc-89 tion as in [1]:  $30 \times 30$  cm square box filled with 2-5 cm thick layer of room-90 temperature liquid metal alloy In-Ga-Sn. To prevent the oxidation of liquid 91 metal and overheating of thin anode electrodes, the gap between the free sur-92 face of the liquid metal and the top anode plate was filled with weak 3% HCl 93 water solution. As the obstacles (further referred to as WB), the identical 94 plexiglass bars of the  $10 \times 15$  mm cross-section, placed across the width of the 95 cell and attached to its bottom, were used. In different tests, their number 96 (from 1 to 7) and the arrangement were changed. Fig. 1a shows schematic 97 view of the experimental cell with only one WB in the middle, while Fig. 1b 98 shows 3D view of the cell with 5 WB uniformly spread along its bottom. 99 The external uniform vertical magnetic field (10...80 mT) generated by two 100 induction coils was applied throughout the cell. 101

The height of WB was kept the same 1.5 cm in all the trials, and was chosen to be less than the minimum height of the liquid metal layer (2 cm) in order not to partition the cell into separate compartments, but to allow the motion of liquid metal across the whole cell.

### $_{106}$ 3 Methodology

The measurements of free surface oscillations in the unstable regime of the cell were taken for different WB configurations and melt heights. Recordings were performed using video camera (Fig.2), which was filming the middle area of the front wall of the cell at 30 fps. This allowed to detect the instantaneous height of the liquid metal at that particular location during the passage of the wave. Later, the video data was post-processed, and the time-history of the surface oscillations extracted with the accuracy of about  $\pm 0.1$  mm.

Before introducing any obstacles in the melt, the test case without them 114 was recorded for every height of the liquid metal layer  $(h_0 = 20, 35, 50 \text{ mm})$ 115 at different values of the anode current I and vertical magnetic field B. This 116 case served as a reference data for later tests with different WB arrangements 117 (Fig.3). Normally, in a single test run for one height of the melt, different 118 WB configurations were tested. To keep the melt level constant, the small 119 amount of In-Ga-Sn alloy was taken out or added into the cell in order to 120 compensate for the volume occupied by WB. 121

The general procedure was the following: the desired WB arrangement was installed in the cell and the required height of the melt was set. The top anode plate with 900 stainless steel electrodes (see Fig.2) was lowered for the tips of the electrodes to immerse into the liquid metal for  $1 \pm 0.25$ mm below the free surface. Then relatively high values of the anode current I and the magnetic field B were set to trigger the onset of the wave.

After that, both I and B were lowered to the desired values. Then the 128 magnetic field was kept constant and the current I was lowered in small 129 steps. At each step of the current magnitude, a video recording of the sur-130 face oscillations was taken. Then the procedure was repeated for a different 131 magnetic field value B, and so on. For each B, a certain minimum value of 132 the anode current  $I_{min}$  was found, at which the cell became stable. This pair 133 of  $B_{min}$  and  $I_{min}$  values was recorded as the 'lower thresholds'. The set of 134 such  $B_{min}$  and  $I_{min}$  combinations was found for each WB arrangement and 135 represented the stability curve, below which the cell is stable. 136

#### <sup>137</sup> 4 Results and discussion

Fig.3 shows the reference case of lower threshold values B and I for when no WB were installed in the cell. The magnetic field was varied between 5 and 80 mT, and the anode current was varied between 100 and 1200 A. The uncertainty of each experimental point on this graph, i.e of finding the lowest  $I_{min}$  value while keeping B constant, is several amperes.

One can see that the curves follow some sort of inverse function  $\sim I^{-1}$  and the higher melt level  $h_0$  generally leads to a more stable cell. The amplitude of the wave is proportional to the product of B and I.

Fig.4 shows the standard deviation of the free surface oscillations, obtained from the video recordings, as a function of the anode current I and the magnetic field B for one height of the melt (35 mm). The amplitude of oscillations grows linearly with respect to the anode current, however its sensitivity to the change in magnetic field B is different: at low B values the growth is close to linear, but then saturates at higher magnetic field.

<sup>152</sup> Now we take the first melt level,  $h_0 = 20$ mm, fix magnetic field at about <sup>153</sup> the midrange B = 50mT, and introduce several WB configurations. Fig.5 <sup>154</sup> shows the obtained surface oscillations with none, one and three WB, ar-<sup>155</sup> ranged in parallel to each other at equal spacings along the width of the cell <sup>156</sup> (as in Fig.1). As seen from the graph, the addition of even one WB lowers the

RMS of oscillations by  $\sim 35\%$  compared to the control case. Three obstacles 157 reduce the RMS by another  $\sim 25\%$ . The last curve in Fig.5 has been obtained 158 with "cross-breaker", which consisted of two single WBs, perpendicular to 159 each other and crossing at the centre of the cell. One can see that such a 160 WB arrangement is damping oscillations most effectively for  $h_0 = 20$  mm, i.e. 161 when the relative height of the obstacle is  $0.75h_0$ . Indeed, because the super-162 position of two sloshing modes along each horizontal direction comprises the 163 overall "rolling" wave, such WB configuration is affecting the sloshing in each 164 of these directions. Finally, Fig.6 shows the lower thresholds of the instability 165 for melt level  $h_0 = 20$  mm. This confirms the gradual improvement of the 166 melt stability from none to one and three WB cases. The "cross-breaker" 167 case, which showed lowest amplitude of the surface oscillations, from the 168 stability point of view, lies somewhat in between 1 and 3 WB arrangements. 169 Stability results for  $h_0 = 35$  mm are shown in Fig.7. Now the relative 170 WB height is  $0.43h_0$  and it is clear that the performance of WB starts to 171 deteriorate: everything below 3 WB has basically no effect on the stability 172 thresholds. Further increase of the number of WB's makes no improvements 173 over 3WB case (we also tested 5WB and 7WB parallel arrangements). 174

Increasing the melt height even further to  $h_0 = 50$  mm, results in almost no influence of WB's on the stability thresholds. The relative WB height now is only  $0.3h_0$ . Fig.8 shows the results of previously most effective 3WB case for this melt level.

The frequency of the free surface oscillations was also found to decrease 179 with the introduction of obstacles in the liquid metal. The frequency spectra 180 of the wave was recovered from the video recordings for two heights of the 181 liquid metal  $h_0 = 20$  and 35 mm. The base frequency for the control case 182 without WB agrees well with the natural frequency of the wave  $f_0$ , which 183 can be easily calculated from the expression for the propagation speed c of 184 the internal gravity waves at the interface between two liquids in a shallow 185 binary layer:  $c = \sqrt{\Delta \rho g}/(\rho_0/h_0 + \rho_1/h_1)$ , where  $\rho_0$  and  $\rho_1$  are densities of 186 the liquid metal and top fluid (water) respectively,  $\Delta \rho$  is their difference, 187 g is the acceleration due to gravity and  $h_1 = 5$ cm is the height of the top 188 fluid. The base frequency  $f_0$ , Hz, of the wave is then obtained as  $f_0 = c/\lambda$ , 189 where  $\lambda = 0.6$  m is the wave length (half of the cell perimeter). Thus, the 190 calculated base frequencies are  $f_0 = 0.66$  Hz for  $h_0 = 20$  mm and  $f_0 =$ 191 0.85 Hz for  $h_0 = 35$  mm. They are in a very good agreement with the ones 192 observed experimentally; see Table 1, which shows experimental values of  $f_0$ 193

<sup>194</sup> for different WB configurations.

#### 195 5 Conclusions

The experimental tests investigating the influence of the different configura-196 tions of "wave-breakers" on the rolling-pad surface instability were performed 197 in the low-temperature laboratory model. The effectiveness of these configu-198 rations was assessed by analysing the data of the stability thresholds and the 199 RMS values of the free surface oscillations. At the high relative height of the 200 obstacles  $(0.75h_0)$  the pronounced suppression of the waves was observed: 201 up to 50% (for 3WB) by RMS value. In this case the frequency of the wave 202 (hence its celerity) was also found to decrease by  $\sim 15\%$  for 3WB and cross-203 WB cases. For the higher melt level  $h_0 = 35$  mm, when the relative height 204 of the obstacles becomes  $0.43h_0$ , the suppression effect was found to be less 205 pronounced, leaving only 3WB configuration as the only one effective: sur-206 face oscillations decreased by  $\sim 30\%$  (RMS) and the wave propagation speed 207 by 8%. Finally, at  $h_0 = 50 \text{ mm}$  (WB height is  $0.3h_0$ ) the damping effect of 208 the obstacles was practically unnoticeable. 209

The outcomes of this study had an important industrial impact: the results were used by Rio-Tinto for the development and validation of the full 3D numerical model of electrolysis cell, which allowed them to increase the productivity of its plants while lowering the environmental footprint. This and the subsequent numerical works [9, 10] led to a patent [11].

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Configuration	$f_0, \text{ Hz} (h_0 = 20 \text{ mm})$	$f_0, \text{Hz}$ $(h_0 = 35 \text{ mm})$
No WB	0.67	0.86
1  WB	0.65	0.84
3  WB	0.58	0.79
$1 \operatorname{cross-WB}$	0.57	0.77

Table 1: Base frequency  $f_0$  of the wave measured for different WB configurations at two heights  $h_0$  of the liquid metal layer.

### <sup>236</sup> Figure Captions



Figure 1: (a) Side view of the experiment with 1 WB installed in the middle of the cell; (b) 3D view of the cell (one side wall removed) with 5 WB equally spaced along its width.



Figure 2: 3D view of the test cell inside the inductor coils.



Figure 3: Lower threshold curves of B(I) for three melt levels  $h_0 = 20, 35, 50$  mm without 'wave breakers'.



Figure 4: RMS value of the surface oscillations vs. anode current I, A for different values of magnetic field B and single melt height  $h_0 = 35$  mm without 'wave breakers'.



Figure 5: RMS value of the surface oscillations vs. anode current I, A for magnetic field B = 50 mT and melt height  $h_0 = 20$  mm with different WB arrangement.



Figure 6: Stability thresholds for melt level  $h_0 = 20$  mm and different WB arrangements.



Figure 7: Stability thresholds for melt level  $h_0 = 35$  mm and different WB arrangements.



Figure 8: Stability thresholds for  $h_0 = 50$  mm: no WB (solid line) and 3WB. Insert shows the 3WB influence on the RMS value of surface oscillations vs. no-WB case for  $h_0 = 50$  mm.