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## The effect of copper doping in $\alpha$ -MnO<sub>2</sub> as cathode material for aqueous Zinc-ion batteries

Rong Lan<sup>\*</sup>, Evangelos Gkanas, Ali Jawad Sahib Sahib, Agata Greszta, Rohit Bhagat, Alexander Roberts

Centre for E-Mobility and Clean Growth, Coventry University, Coventry CV1 2TL, United Kingdom

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Keywords: Manganese Dioxide Copper Doping Cathode Materials Zinc-ion Batteries	Copper-doped Manganese Dioxide has been synthesised through a simple hydrothermal method at different doping levels. The synthesised materials have been characterized by X-ray diffraction (XRD), and scanning electron microscopy (SEM) to determine the composition, structure, and morphology. All the Cu doped MnO <sub>2</sub> ar found to be single phased. Their electrochemical properties as cathode for Zinc-ion batteries are studied by cycli voltammetry (CV), galvano-static charge / discharge (GCD) and electrochemical impedance spectroscopy (EIS) using 3 M ZnSO <sub>4</sub> + 0.3 MnSO <sub>4</sub> solution as the electrolyte. 3.8% Cu doped MnO <sub>2</sub> has shown the highest initia capacity of 379.5 mAh g <sup>-1</sup> at 0.02 A·g <sup>-1</sup> , and 304.4 mA h g <sup>-1</sup> at 0.5 A g <sup>-1</sup> , but experienced fast fading with poor capacity retention of 56.8% after 100 cycles. 7.4% Cu doping gives lower capacity, while 5.9% dopin shows a higher discharging capacity (320.0 mAh·g <sup>-1</sup> at 0.02 A·g <sup>-1</sup> and 269.3 mAh·g <sup>-1</sup> at 0.5 A·g <sup>-1</sup> ) an improved stability (85.8% capacity retention after 100 cycles), better than non-doped MnO <sub>2</sub> electrode (284. mAh g <sup>-1</sup> at 0.02 A g <sup>-1</sup> and 252.1 mAh·g <sup>-1</sup> at 0.5 A g <sup>-1</sup> , capacity retention 76.7%). The samples show satis factory capacity and rate capability while the cycling stability is not ideal, which may relate to the needle lik morphology and nanoscale particle size. CV tests revealed that the electrochemical process is mainly diffusion controlled. The zinc ion diffusion coefficient is tested to be in the range of 10 <sup>-12</sup> cm <sup>2</sup> ·s <sup>-1</sup> from both CV and EI tests and showed the same trend in their electrochemical reversibility, as evidenced by the reduction of the redo peak potential difference from 0.31 to 0.24 V at 1.1 mV·s <sup>-1</sup> , and from 0.45 V to 0.31 V at 5 mV·s <sup>-1</sup> . Whilst th cell resistance of non-doped MnO <sub>2</sub> increased from 1.78 $\Omega$ to 7.39 $\Omega$ after cycling. These results indicate tha Cu-doping is effective to increase the conductivity of the materials, reduce the polarization during charge and discharge, and improve the cycling stability of			

#### 1. Introduction

Aqueous batteries, or water-based batteries, offer several benefits compared to traditional non-aqueous (organic electrolyte) batteries, especially in safety, environmental benignity, and cost-effectiveness [1–3]. Among them, aqueous Zinc-ion batteries (ZIBs) are the most investigated [4–6]. ZIBs are promising for large-scale energy storage applications [1–4] e.g. grid-level energy storage systems, because their manufacturing processes are relatively simple with less constraints, and the materials used are widely available. While zinc-ion batteries have several advantages, they also face significant challenges to be addressed before their commercial implementation. Current ZIBs have a shorter

cycle life compared to other battery technologies with the repeated insertion and extraction of zinc ions during charging and discharging cycles causing the electrodes to undergo structural changes and degrade over time, limiting the number of cycles the battery can withstand. ZIBs typically operate at a lower voltage compared to other battery chemistries which limits their application in devices or systems that require higher voltage levels. While ZIBs can offer high energy density compared to other aqueous batteries, they generally have lower energy density compared to lithium-ion batteries (LIBs). ZIBs have slower kinetics, leading to limited charge/discharge rates and lower power capabilities. [7]

Improvement in electrode materials (both anode [8–10] and cathode

\* Corresponding author. *E-mail address:* rong.lan@coventry.ac.uk (R. Lan).

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[6,11–15]), electrolyte formulation [5,16–20] interface regulation and battery designs [21-23] are the key to addressing these limitations. Manganese dioxide (MnO<sub>2</sub>) is the most commonly used cathode material in ZIBs [24-28], with some favourable characteristics [29], but challenges remain including: (1) Low conductivity: MnO<sub>2</sub> is inherently a poor electronic conductor, resulting in higher internal resistance, lower power output, and reduced columbic efficiency. (2) Large volume expansion: MnO2 experiences significant volume expansion and contraction during charging and discharging, leading to mechanical stress with cracking and self-pulverisation resulting ion loss of cycle life. (3) Irreversible side reactions: MnO2-based cathodes can experience irreversible reactions during cycling, resulting in a reduced reversible capacity and overall energy storage capability of the cell. (4) Formation of surface layers: the formation of insulating layers on the surface of the cathode material can occur during cycling, hampering the ion diffusion and electron transport. [30] (5) Limited voltage range: MnO<sub>2</sub>-based cathodes typically operate within a limited voltage range, which can restrict the energy storage capacity and application range of the battery, not suitable for high-voltage applications where higher energy densities are required. Strategies have been proposed to solve above problems [31], such as atomic engineering [32], nano-structuring the MnO<sub>2</sub> material[33], incorporating conductive additives[34], and optimizing electrolyte composition[35] to enhance the conductivity, stability, and cycling performance of the cathode. These efforts aim to improve the overall performance and viability of MnO2-based ZIBs for various applications.[36]

Since 2021, doped MnO<sub>2</sub> has been an area of active research and development in the field of energy storage. Various dopants, including transition metals (e.g., Fe, Co, Ni) [37-43], non-metals (e.g., N, F, S) [44-50], and carbon-based materials [51,52], have been studied for doping MnO<sub>2</sub>. Doping can enhance the electron transport, mitigate the low conductivity issue associated with pure MnO2, and improve the cycling stability [45,46,53,54]. It can also reduce the volume expansion and contraction of MnO2 during cycling, mitigating the mechanical stress and strain that lead to material degradation [45,46,48]. Doping strategies have been investigated to expand the voltage range of MnO<sub>2</sub>-based cathodes. By incorporating specific dopants, researchers aim to extend the operating voltage of MnO<sub>2</sub> beyond its intrinsic limit. This expansion can enable higher energy densities and make doped MnO<sub>2</sub> suitable for applications requiring increased voltage levels. The choice of dopant and doping method depends on the desired improvements in conductivity, stability, and electrochemical performance. Doping methods include chemical synthesis routes [30,49], electrochemical deposition [55–58], and chemical / physical vapour deposition techniques[59,60]. The development and optimization of doped MnO<sub>2</sub> cathodes in energy storage applications are ongoing, with new research findings and progresses continually emerging.

Copper-doped MnO<sub>2</sub> refers to the incorporation of copper ions  $(Cu^{2+})$  into the crystal structure of MnO<sub>2</sub> [61]. This doping process involves substituting some of the Mn atoms with Cu atoms, altering the composition and properties of MnO<sub>2</sub>. Copper doping in MnO<sub>2</sub> can increase the overall conductivity by facilitating charge transport within the crystal lattice. Copper doping has the potential to enhance the electrochemical performance of MnO<sub>2</sub>, including the reversible capacity, cycling stability, and rate capability, making it more suitable for energy storage applications. Doping with copper ions can influence the structural stability of MnO<sub>2</sub> by mitigating the volume expansion and contraction issues, improving the cycling stability and prolonging the material's lifespan. The extent of copper doping in MnO<sub>2</sub> can vary depending on the desired properties and specific applications. The doping level needs to be carefully controlled to balance the conductivity enhancement and maintain the structural integrity of the material.

Copper-doped  $MnO_2$  can be synthesized through various methods, such as solid-state reaction, hydrothermal synthesis, or sol-gel methods. The choice of synthesis method affects the homogeneity, purity, and overall properties of the doped material. Copper-doped  $MnO_2$  has

potential applications in various electrochemical devices including fuel cells [62,63] and metal air batteries [64,65], including lithium-ion batteries [61,66-68], Zinc-ion batteries [38,69-74], supercapacitors [75-78], and hybrid capacitors. It is also explored for catalytic and electrochemical sensing applications due to its modified properties [79-83]. Cu doped MnO<sub>2</sub> through a wet-chemical method was studied as the potential cathode materials for Lithium-ion batteries. [61] The doping effect was investigated on the improvement for the magnetic and electrical properties. Cu-intercalated  $\delta$ -MnO<sub>2</sub> was obtained through an ion exchange treatment by immersing  $\delta$ -MnO<sub>2</sub> powders in CuSO<sub>4</sub> solution, with MnO<sub>2</sub> synthesised through hydrothermal reaction[69]. Copper doping at different levels is not studied. Binder-free Cu-doped  $\epsilon$ -MnO<sub>2</sub> has been synthesized through electrodeposition, when copper is co-deposited with MnO<sub>2</sub>. [56] The best performance from this research came from the sample deposited on Carbon Nano Tube (CNT) film. Sputtered Cu on MnO<sub>2</sub> also showed a good performance in Zinc-ion batteries. From these previous research, Copper doped MnO2 is a promising cathode for Zinc-ion batteries.

Different doping levels, synthesis techniques, and characterizing the performance of copper doped  $MnO_2$  in battery systems and other energy storage applications still need to be investigated. In this paper, copper doped  $MnO_2$  was synthesised through a simple hydrothermal process, and was investigated as the cathode material for ZIB, aiming to optimize the doping level for better properties and performance of  $MnO_2$  for practical and efficient use in aqueous ZIBs.

#### 2. Experiments

#### 2.1. Materials

KMnO<sub>4</sub> (99%, Thermo Scientific Chemicals), MnSO<sub>4</sub> (99+%, Thermo Scientific Chemicals), CuSO<sub>4</sub> (>99.0%, Acros Organics, UK), 1-Methyl-2-pyrrolidinone (NMP, 99+%, Thermo Scientific Chemicals) Zinc foil (99.98%, thickness 1 mm, Alfa Aesar), glass fibre (GF6, Whatman), are purchased from Fisher Scientific, UK. Poly (vinylidene fluoride) (PVDF), and carbon black were purchased from GELON LIB GROUP, China.

#### 2.2. Preparation of MnO<sub>2</sub>

0.227 g MnSO<sub>4</sub> were dissolved in a beaker containing 10 ml deionised (DI) water under magnetic stirring for 10 minutes at 400 rpm. Calculated amount of CuSO<sub>4</sub> according to the molar ration to the final MnO<sub>2</sub> at 10%, 20%, and 30% was added and was kept stirring until fully dissolved. 10 ml KMnO<sub>4</sub> (0.1 M) was added to the above solutions slowly under stirring. The mixture was kept in ultrasonic bath for 0.5 h before being moved to an autoclave with a 30 ml Teflon liner, then reacted at 120 °C for 12 hours. After cooling the product to room temperature, it was then centrifugally washed with deionized water, and dried under vacuum at 60 °C for 12 hours. The collected powder was then calcined at 400 °C for 2 hours. The obtained samples are referred to as MC0 for nondoped MnO<sub>2</sub>, and MC1 MC2 and MC3 for Cu doped MnO<sub>2</sub> from low to high doping level, individually.

#### 2.3. Characterization

#### 2.3.1. Morphology and chemical phase analysis

X-ray diffraction (XRD) tests were performed on a Bruker D8 Advance Diffractometer in Bragg-Brentano geometry with Cu K $\alpha$  radiation  $\lambda = 1.5404$  Å and a diffracted beam graphite monochromator. Powder X ray diffraction data is recorded for the 2 $\theta$  angle range between 20° and 90° at room temperature with step size 0.0495° at 15 s per step. The observed XRD data is indexed with powder X software[84] and then subjected to Rietveld refinement with GSAS II [85]. Morphology and elemental composition of the materials were characterised using scanning electron microscopy (SEM) (1530 VP Field Emission Gun Scanning Electron Microscope (FEG-SEM), Carl Zeiss, Germany) and energy dispersive X-ray spectroscopy (EDS) (X-MAX EDX, Oxford Instruments, UK).

#### 2.3.2. Electrochemical analysis

The electrochemical performances of MC0, MC1, MC2, MC3 cathodes for aqueous ZIBs were investigated in CR2032 coin cells. The asprepared MnO<sub>2</sub> samples were used as electrode active material. They were mixed with carbon black and poly (vinylidene difluoride) in an 8:1:1 wt ratio and dispersed in N-methyl-2-pyrrolidone solvent. The obtained ink was transferred onto stainless steel mesh substrate and then dried at 80 °C for 10 hours. The casted electrode was then cut into disks of a diameter of 1.6 mm, with a final mass loading of 1.4 1.5 mg cm<sup>-2</sup>. CR2032 coin cells are assembled using the as prepared MnO2 cathode, polished zinc foil anode (99.98%, thickness 1 mm, Alfa Aesar), glass fibre as separators (GF6, Whatman), and 3 M ZnSO<sub>4</sub> + 0.3 M MnSO<sub>4</sub> solution as electrolyte.

Electrochemical performances of the as-assembled CR2032 full cells were assessed through Electrochemical Impedance Spectroscopy (EIS), Cyclic Voltammetry (CV), and Galvanostatic Charge / Discharge (GCD) cycling using a VMP3 multi-potentiostat (Bio-Logic Science Instruments SAS, France, EC-Lab software). All the electrochemical performance was tested at 25 °C. The voltage window of GCD and CV tests were 1–1.8 V. CV scanning tests were carried out at 0.1–5 mV s<sup>-1</sup>, respectively, with GCD at current densities between 0.02 and 0.5 A g<sup>-1</sup>, and EIS at a frequency range from  $10^{-2}$  to  $10^{6}$  Hz, at a perturbation amplitude of 10 mV.

#### 3. Results and discussions

#### 3.1. SEM tests of the non-doped and copper doped MnO<sub>2</sub>

Fig. 1 shows the morphology of the synthesised  $MnO_2$  materials from scanning electron microscopy (SEM), presenting needle-like primary particles with width of 20–50 nm and length of 400–800 nm. The size of the nano-needles seems to be reducing slightly with the doping of copper increases. Energy dispersive X-ray spectroscopy (EDS) analysis shows



Fig. 1. SEM image of the synthesised MnO2 at different copper doping: a), b), c) MCO; d), e), f) MC1; g), h), i) MC2; j), k), l) MC3.

even distribution of the elements and indicates that the copper doping level is significantly lower than expected, which turns out to be 3.82% of Cu for MC1, 5.89% of Cu for MC2 and 7.43% of Cu for MC3, in molar percentage.

#### 3.2. XRD characterisation of the cathode materials

Powder X-Ray diffraction was used to examine the phase and crystallinity of the prepared samples. All samples exhibit identical sharp diffraction peaks, which can be indexed to the pure tetragonal phase of  $\alpha$ -MnO<sub>2</sub> (JCPDS No. 00–44–0141.), space group I4/m. The XRD results indicate that all the samples are single phase as shown in Fig. 2, which has been further confirmed by retrieved refinement. The refined XRD pattern is shown in Fig. 3.

The refined lattice constants are listed in Table 1 and shown in Figure S1. As compared with the reported lattice parameters of  $\alpha$ -MnO<sub>2</sub>, a = b = 0.9785 nm and c = 0.2863 nm (ICSD: 44–141), in general the lattice parameters a / b increased with increasing level of copper doping. While c decreased slightly in MC1, it increased in MC2 and MC3. Since the valance state of Cu is lower than Mn, doping of copper will introduce oxygen vacancies into the lattice, which causes the lattice constant to reduce slightly. With higher doping, the oxygen vacancies increase, and the metal – oxygen bonding become weaker, which leads to the increase of the lattice constants. The lattice expansion due to doping indicates loosened lattice constraints in the nanostructures.

The particle size of the samples was also calculated from Sherrer's equation [86,87].

$$D = \frac{K \times \lambda}{\beta \cos \theta} \tag{1}$$

Where D is the particle size, K is a dimensionless shape factor, here we use K = 0.9.  $\lambda$  is the wavelength of CuK $\alpha$ 1, which is 1.5406 Å.  $\beta$  is the line broadening at half the maximum intensity (FWHM), after subtracting the instrumental line broadening, in radians.  $\theta$  is the Bragg angle. The particle size listed in Table 1 is based on the data at the strongest (211) peak at  $2\theta \approx 37.5^{\circ}$ . The calculated particle size is in the range of 80–110 nm, which is fairly closed to the value observed by SEM (Fig. 1).

The theoretical density is calculated using the following equation,

$$\rho = \frac{1.66 \times Z \times MW}{V} \tag{2}$$

Where  $\rho$  is the theoretical density, Z is the number of molecules in each unit cell, MW is the molecular weight in g mol<sup>-1</sup>, V is the lattice volume



Fig. 2. XRD patterns of the synthesised  $\rm MnO_2$  samples with different level of copper doping.

in Å<sup>3</sup>. For  $\alpha$ -MnO2 with spece group I4/m (87), Z = 8. The calculated theoretical density of the four samples are listed in Table 1. With the increased doping level of copper, the theoretical density gradually increases from sample MC0 to MC3.

The surface area was calculated using the following equation, [86, 88–92]

$$S = \frac{6000}{D \times \rho} \tag{3}$$

Where S is the surface area,  $m^2/g$ , D is the particle size,  $\rho$  is the theoretical density. The calculated surface area for the four samples are also listed in Table 1. The copper doped samples have slightly higher surface area than undoped MnO<sub>2</sub>.

The crystallinity percentage of the samples is calculated by the following equation [86].

$$% Crystallinity = \frac{A_{cp}}{A_{ta}} \times 100 \tag{4}$$

Here, Acp is the area under crystalline peaks, Ata is the total area of the XRD peaks.

#### 3.3. Cyclic Voltammetry tests of the zinc-ion batteries

To investigate the kinetics, cyclic voltammetry (CV) method [93] was applied at different sweep rates of 0.1-5 mV/s with a voltage range of 1.0-1.8 V versus Zn<sup>2+</sup>/Zn in assembled CR2032 coin cells. Fig. 4 shows the CV tests before and after the cell cycling. Fig. 4a) shows the CV tests at 0.1 mV/s. In the reduction scan from 1.8 V to 0.8 V, two peaks appear at around 1.4 V and 1.3 V vs.  $Zn/Zn^{2+}$ , which can be attributed to  $Zn^{2+}$  or  $H^+$  ions insertion into the  $MnO_2$  host structure. [94] The oxidation scan towards 1.8 V also presented a peak at approximately 1.55 V vs. Zn / Zn<sup>2+</sup>, corresponding to the oxidation of  $Mn^{3+}$  back to  $Mn^{4+}$  and the de-insertion of  $Zn^{2+}$  ions. The CVs at a scan rate of 0.1 mV s<sup>-1</sup> appeared to be stable and consistent. CV curves are well overlapped, indicating good reversibility of cathode, except for the slight reduction of the peak current at 1.3 V, which reveals a decreased contribution to the capacity from H<sup>+</sup> ions. This could be caused by the high pH value of the electrolyte that limited the supply of H<sup>+</sup> ions. In the cathodic/anodic scans, the redox peaks appeared at the same location for all the cathodes, evidencing that Cu doped cathodes possess similar redox reactions to MnO<sub>2</sub> cathode, and does not significantly affect the electrochemical process or storage mechanism of MnO<sub>2</sub>,[21]

The CV results at 0.1 mV of the samples showed that doping reduced the redox peak potential differences. With copper doping, the oxidation peaks shifted to the left while the reduction peaks shifted to the right, which brings down the redox peak potential difference from 0.19 to 0.16 V at 0.1 mV·s<sup>-1</sup> scanning speed, from 0.29 V to 0.26 V at 1.1 mV·s  $^{-1}$  scanning speed, and from 0.41 V to 0.30 V at 5 mV s  $^{-1}$  scanning speed (Fig. 5). After cycling, the reduction in redox peak potential difference became more significant. As shown in Fig. 5, the peak potential difference is smaller at low scan rate and became even bigger at higher scanning rate, compared to the trend of the results from the fresh cells. It comes down from 0.20 V to 0.18 V at 0.1 mV $\cdot$ s<sup>-1</sup> scanning speed, from 0.31 V to 0.23 V at 1.1 mV s^{-1} scanning speed, and from 0.45 V to 0.30 V at  $5 \text{ mV} \cdot \text{s}^{-1}$  scanning speed. All the copper doped samples showed similar reduction in the redox peak potential difference despite that their doping levels are different. After cycling, the redox peak potential difference for MC0 (non-doped) increased from 0.19 V to 0.20 V at 0.1 mV·s  $^{-1}$  , from 0.29 V to 0.31 V at 1.1 mV·s  $^{-1}$  , and from 0.41 V to 0.45 V at 5 mV s  $^{-1}$ ; whilst for the doped samples, the redox peak potential difference increased from 0.16 V to 0.18 V only at 0.1 mV s<sup>-1</sup>, but reduced from 0.26 V to 0.23 V at 1.1 mV s  $^{-1}$ , and from 0.45 V to 0.41 V at 5 mV s  $^{-1}$ , after cycling. These results indicate that copper doping has effectively reduced the polarization on the electrode.

A dominating pair of redox peaks exhibits increasing currents when



Fig. 3. XRD Rietveld refinement (GSAS II) patterns of the non-doped and copper doped MnO<sub>2</sub> samples: a) MCO; b) MC1; c) MC2; d) MC3.

Table 1Key crystallographic parameters and grain properties of the samples.

Sample	Composition	Lattice parameters		Particle size (nm)	Theoretical density (g $\rm cm^{-3}$ )	Sur-face area (m <sup>2</sup> /g)	Crystallinity (%)	
		a (Å)	C (Å)	V (Å <sup>3</sup> )				
MC0	MnO <sub>2</sub>	9.8232(3)	2.8624(5)	276.21(5)	111.06(2)	4.1798(4)	12.92(4)	88.1
MC1	Mn <sub>0.962</sub> Cu <sub>0.038</sub> O <sub>2-δ</sub>	9.8310(4)	2.8647(2)	276.87(3)	86.89(8)	4.1855(1)	16.49(6)	83.3
MC2	Mn <sub>0.941</sub> Cu <sub>0.059</sub> O <sub>2-δ</sub>	9.8330(2)	2.8642(9)	276.94(3)	79.17(7)	4.1931(1)	18.07(2)	84.0
MC3	$Mn_{0.926}Cu_{0.074}O_{2\text{-}\delta}$	9.8338(8)	2.8653(8)	277.09(7)	81.23(7)	4.1969(7)	17.59(7)	86.3

the sweep rates increase. The electrodes do not present a capacitive behaviour of the electrode. The capacitive effect is characterized by analysing the cyclic voltammetry data at different sweep rates as in Eq. (5) [93]:

$$i = av^b \tag{5}$$

In which i is the specific peak current,  $\nu$  is the potential sweep rate, and a, b are parameters that can be fitted from the experimental data. Eq. (1) can be taken with logarithm and can be expressed according to Eq. (2):

$$lni = lna + blnv \tag{6}$$

The b value is the slope of the linear fitting of lni versus ln $\nu$ . When b value is close to 1, the system is mainly capacitance controlled; when b value is close to 0.5, the Zn<sup>2+</sup> ion insertion process dominates with the redox reaction limited by the diffusion-controlled behaviour. Figure S5 shows the ln i versus ln  $\nu$  plots at oxidation and reduction process of the cyclic voltammogram.

The bo (oxidation process) and  $br_{Zn}$  (reduction process of  $Zn^{2+}$ 

peak)  $br_H$  (reduction process with  $H^+$  de-escalation) of the cathodes, obtained from the above fitting (plotted in Figure S5) are listed in the Table 2.

The average b values are close to 0.5, which implies that the redox reactions on cathodes are controlled by the diffusion process.  $MnO_2$  is a transition metal oxide that typically displays the pseudo-capacitance behaviour [95]. The capacitive-controlled process occurs only on the surface. However, our  $MnO_2$  samples turned out to be mainly diffusion-controlled processes. This means, the insertion/extraction of ions occur not only on the surface but also the bulk. The result suggested a fast  $Zn^{2+}$  ion insertion/extraction or high-rate property for the battery.

When the process is diffusion controlled, the diffusion coefficient can be estimated from CV through Randles-Sevcik (Eq. (7)) to calculate the peak current ( $i_p$ ) using scan rate ( $\nu$ ) in an observed voltammogram. For redox reaction cycles, peak current ( $i_p$ ) depends on the concentration C, the diffusion coefficient (D), the scan rate ( $\nu$ ), and the electrode surface area (A) of redox-active species. [96,97]



Fig. 4. CV test of the coin cells before and after cycling: a) at 0.1 mV·S<sup>-1</sup>; b) at 1.1 mV·S<sup>-1</sup>; a) at 5 mV·S<sup>-1</sup> a) at 0.1 mV·S<sup>-1</sup> after cycling; a) at 1.1 mV·S<sup>-1</sup> after cycling; a) at 1.1 mV·S<sup>-1</sup> after cycling.

$$i_p = 0.4463 \left(\frac{n^3 F F^3}{RT}\right)^{1/2} A \bullet C \bullet (D \bullet v)^{1/2}$$
(7)

Where  $i_p$  is the Peak current (amperes), n is the Number of electrons transferred in a redox cycle, F is Faraday's constant (96485 C·mol<sup>-1</sup>), R is the Universal gas constant (8.3145 J·K<sup>-1</sup> ·mol<sup>-1</sup>), T is Absolute temperature, A is the electrode surface area in working (cm<sup>2</sup>), C is the Molar concentration of redox-active species (mol·cm<sup>-3</sup>), D is the diffusion coefficient (cm<sup>2</sup> s<sup>-1</sup>),  $\nu$  is the scan rate in V·s<sup>-1</sup>. The calculated diffusion efficiencies (D) are in good agreement with their electrochemical

performance in coin cells, with MC1 exhibits the highest D before cycling. The diffusion coefficient data are presented in Fig. 11 together with those data deduced from EIS tests.

#### 3.4. Rate and cycling tests of the zinc-ion batteries

Fig. 7 shows the rate performances of  $MnO_2$  cathodes, at various specific current densities of 20, 50, 100, 200, and 500 mA·g<sup>-1</sup>. The capacities of MC1 and MC2 are much higher than non-doped MnO<sub>2</sub>. At a higher doping level, the electrochemical performance of MC3 is lower



**Fig. 5.** Redox peak potential difference from CV tests of the coin cells before and after cycling: a) the potential difference between anodic peak and the cathodic peak of  $Zn^{2+}$ ; b) the potential difference between anodic peak and the cathodic peak of  $H^+$ ; c) the potential difference after cycling between anodic peak and the cathodic peak of  $Zn^{2+}$ ; d) the potential difference between anodic peak and the cathodic peak of  $H^+$ .



Fig. 6. a) CV tests of the coin cells at 5 mV rate before and after cycling; b) Redox peaks potential difference of the coin cells after cycling, under varied scan rate of 1  $\sim$  5 mV/s.

than the non-doped  $MnO_2$  sample. When cycled at a specific current density of 200 mA·g<sup>-1</sup>, MC2 delivered a discharge capacity of 276 and charge capacity of 298 mAh·g<sup>-1</sup>. The rate capability and capacity are satisfactory when compared to other reports [69,72,74].

The cycling tests are carried out at 200 mA·g<sup>-1</sup>. The columbic efficiencies are around 99%. MC2 performed the best among all the samples. The capacity retention is 76.7% for MC0. MC1 experienced fast fading with a poor capacity retention of 56.8% after 100 cycles. It was

#### Table 2

The slope of the linear fitting of lni versus  $ln\nu,$  from the CV tests on coin cells.

		MC0	MC1	MC2	MC3
Fresh cells	bo	0.589	0.466	0.459	0.491
	$b_{r-Zn}^{2+}$	0.771	0.768	0.718	0.705
	$b_{r-H}^+$	0.505	0.468	0.416	0.425
Cycled cells	bo	0.523	0.502	0.491	0.494
	$b_{r-Zn}^{2+}$	0.620	0.565	0.594	0.597
	$b_{r-H}^+$	0.647	0.612	0.562	0.590

85.8% for MC2 and 74.7% for MC3. This behaviour indicates that the Cu doped  $MnO_2$  are promising candidates for the  $Zn^{2+}$  ion storage material. This suggests that optimized level of Cu doping could improve both the cycling and rate performance as well as the stability for ZIBs. The cyclability is not ideal, which could be related to their needle-like morphology and nanoscale particle size as shown in Fig. 1. Further investigation on Cu doped  $MnO_2$  with different particle morphology could be helpful.



Fig. 7. The rate and cycling performances of full zinc-ion coin cells using different MnO<sub>2</sub> cathodes (non-doped and different level of copper doping): a) initial rate performance; b) rate tests of MC0; c) rate tests of MC1; d) rate tests of MC2; e) rate tests of MC3; f) cycling tests.

#### 3.5. EIS tests of the zinc-ion batteries before and after cycling

Fig. 8 displaces EIS results. The curves consist of depressed semicircles and diffusion drift which can be fitted using the equivalent circuit as shown in Fig. 9, where Rs, Ri, Rct, CPE, and Zw represent series resistance, interfacial resistance between the electrolyte and electrode, charge transfer resistance, constant phase element, and Warburg diffusion process, respectively.

The Rct value from EIS fitting are shown in Table 2. MC1 showed the lowest Rct before cycling, and MC2 gave the lowest Rct after cycling, which is in good agreement with the electrochemical performance before and after cycling. It is noted that, the charge transfer resistances are high, which agrees with the low diffusion coefficients as calculated, which is also believed to be the main reason of the not very satisfying cycling performance in this research. It can be solved by improving the electrical conductivity of the samples through constructing a conductive support using the graphite, while preparing the cathode active materials. If as synthesized  $\alpha$ -MnO<sub>2</sub> are dispersed on graphite, it will increase the contact area between the electrode and the electrolyte and provides more electrochemically active sites for ion-insertion, which can hopefully also enable higher rate performance.

The relationship between real impedance (Z') and angular frequency ( $\omega$ ) in the low frequency region can be expressed accordingly as follows [97]:

$$Z' = Rs + Ri + Rct + \sigma \omega^{-1/2} \tag{8}$$

 $\sigma$  is the Warburg factor which is relative to Z'-  $\omega^{-1/2}$  obtained from the slope of the lines as shown in Fig. 10.

The diffusion coefficient of zinc ion can be calculated as in the following equation [98–101]:

$$D = R^2 T^2 / 2A^2 n^4 F^4 C^2 \sigma^2$$
(5)

R is the gas constant, T is the absolute temperature, n is the number of electrons per molecule oxidized (2 for Zinc ions), A is the surface area, F is Faraday's constant, C is the concentration and D is the diffusion coefficient.

The calculated diffusion coefficients of Zinc ions from EIs are in good agreement with the results from CV tests, although slightly lower, due to the testing technique. The diffusion coefficient of samples with higher copper doping - MC2 and MC3 both increased after cycling. Among them MC1 showed highest diffusion before cycling, which is consistent with the cell performance at the beginning of cycling tests. After cycling MC2 gives the highest diffusion coefficient which also matches the results from cycling tests.



Fig. 9. Equivalent circuit.

Table 3	
Rct value from	EIS fitting.

	MC0	MC1	MC2	MC3
Rs (Ω)-Fresh	1.742	1.976	2.646	7.39
Rs (Ω)-Cycled	6.637	1.172	2.392	1.779
Ri (Ω)-Fresh	0.699	0.803	0.946	1.118
Ri (Ω)-Cycled	1.921	3.252	1.342	1.305
Rct (Ω)-Fresh	344.5	267.2	359.6	526.5
Rct (Ω)-Cycled	871.6	782.6	529.1	812.6

#### 4. Conclusions

Homogenous Copper-doped Manganese Dioxide has been synthesised and investigated as cathode materials for ZIBs with different doping levels. All the Cu doped MnO2 are found to be single phase  $\alpha$ -MnO<sub>2</sub>. Their electrochemical properties as cathode for Zinc-ion batteries are studied. Their pseudo-capacitive behaviour has been investigated, which reveals that charging/discharging processes after cycling are diffusion controlled, while the discharging in fresh cells is a combined process with both capacitive and diffusion contributions. MC2 is found to be the optimum doping level, gives improved performance and better stability, when compared to non-doped MnO2 samples. MC1 has shown the highest initial capacity of 379.5 mAh·g<sup>-1</sup> at 0.02 mAh·g<sup>-1</sup> rate, but it experienced fast fading with a capacity retention of 56.8% after 100 cycles. MC3 showed the lowest capacity among all the samples, suggesting higher level of does not give more benefits. The MC samples showed satisfactory electrochemical properties such as higher capacity and better rate capability, while the non-ideal cyclability could be related to their needle-like morphology and nanoscale particle size. The zinc ion diffusion coefficient of all samples before and after cycling are tested to be in the range of  $10^{-12}$  cm s<sup>-1</sup> with a good consistency with their according cell performances, using both cyclic voltammetry and electrochemical impedance spectroscopy. The redox peak difference has been notably reduced, at a similar level for all copper doped samples, compared to non-doped MnO2. It was noticed that the cell



Fig. 8. EIS test of the coin cells a) before and b) after cycling.



Fig. 10. Warburg factor from Z'-  $\omega^{-1/2}$  plot: a) cells before cycling; b) cells after cycling.



Fig. 11. Diffusion coefficients from CV and EIS tests before and after cycling.

Table 4

Diffusion coefficient from EIS tests.

Diffusion coefficient ( $10^{-12} \text{ cm}^2 \cdot \text{S}^{-1}$ )	MC0	MC1	MC2	MC3
D fresh	2.202	5.024	2.342	1.006
D cycled	2.429	2.318	4.353	3.057

resistance of non-doped MnO<sub>2</sub> increased from 1.78  $\Omega$  to 7.39  $\Omega$ , while the cell resistance of Cu-doped cathode all experienced slight reduction during cycling. The results from this paper suggested that Cu-doping is effective to reduce the polarization during charge-discharge, to reduce the resistance, and improve the cycling stability of MnO<sub>2</sub>. In this report, the doping level of copper in MnO<sub>2</sub> from hydrothermal process is significantly lower than that in the prepared precursor. Further effort is required to investigate copper doping at higher levels for further investigation. Suitable supporting conductive materials with implementation of nanomaterials such as carbon nanotubes or graphene, could be helpful to improve the Zn<sup>2+</sup> diffusion. New processes of materials synthesis, supporting conductive materials or second doping could be considered to improve the capacitive behaviour of the cathode materials.

#### CRediT authorship contribution statement

Alexander Roberts: Writing – review & editing. Rohit Bhagat: Resources, Funding acquisition. Agata Greszta: Investigation. Ali Jawad Sahib Sahib: Investigation. Evangelos Gkanas: Writing – review & editing, Supervision. Rong Lan: Writing – review & editing, Writing – original draft, Supervision, Methodology, Investigation, Conceptualization.

#### **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

#### **Data Availability**

Data will be made available on request.

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#### Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.jallcom.2024.174528.

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